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# Alkali-activated materials for radionuclide immobilisation and the effect of precursor composition on Cs/Sr retention

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## **Abstract**

One of the major challenges for the nuclear industry is the safe and sustainable immobilisation of radioactive wastes (RAW). Currently, the most commonly used immobilisation matrices for low and intermediate level wastes are based on ordinary Portland cement. For the more difficult to immobilise nuclides, such as caesium ( $\text{Cs}^+$ ) and strontium ( $\text{Sr}^{2+}$ ), researchers have been studying alternative immobilisation matrices, of which alkali-activated materials (AAM) are a very promising option. However, the differences in precursor compositions and the use of different types of activating solutions make it difficult to fully understand the effects of precursor composition on the immobilisation of introduced nuclides. Therefore, six different compositions of laboratory-synthesized Ca-Si-Al slags were developed to serve as precursors for low-alkaline AAMs to study their immobilisation behaviour. Immobilisation capacities up to 97.6 %  $\text{Cs}^+$  and 99.9 %  $\text{Sr}^{2+}$  were achieved with 1 wt% waste loading when leaching for 7 days at 20 °C in Milli Q water.  $\text{Cs}^+$  immobilisation is higher at lower Si/Al and Ca/(Si+Al) ratios. Immobilisation of  $\text{Sr}^{2+}$  is higher at a lower Ca/(Si+Al) ratio and independent of Si/Al ratio. The results of this study offer a deeper understanding of the immobilisation behaviour of AAMs and can encourage further research and application of AAMs for RAW immobilisation.

## **Keywords**

**Alkali-activated material; immobilisation; radioactive waste; caesium; strontium**

## **1 Introduction**

In the pursuit of a sustainable society, one of the main challenges for researchers and industries is the safe management and disposal of industrial wastes, with radioactive waste (RAW) being particularly important. RAW is produced by many different sources; the main ones being the energy sector (nuclear fuel cycle), the dismantling of nuclear installations, and applications in medicine,

agriculture and industry. Because of the ever-increasing amounts of RAW, continuous innovation in immobilisation is becoming more and more important. As an alternative to the currently widely used cementitious immobilisation matrices, alkali-activated materials (AAM) have been increasingly studied. Depending on the type of precursor and the composition of the hydration products, AAMs (or subclasses thereof) are also known as geopolymers, inorganic polymers, soil cements, geocements, alkaline cements, zeoceramics, alkali-activated slag cement and a variety of other names [1,2]. AAMs have demonstrated promising results in immobilising radionuclides such as caesium and strontium [3-22]. As an example, the superior  $\text{Cs}^+$  retention of AAMs was reported by *Shi and Fernández-Jiménez* (2006) [9], who tested leaching of  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  from AAMs containing zeolites and/or metakaolin (MK) as additives. They concluded that wastes show much less interference with the hydration of AAMs than that of ordinary Portland cement. *Blackford et al.* (2007) [11] developed a geopolymer matrix derived from MK, in which  $\text{Cs}^+$  was introduced. They concluded that  $\text{Cs}^+$  was fully incorporated into the amorphous geopolymer phase, proving the potential of AAMs for RAW immobilisation. In addition to the immobilisation of  $\text{Cs}^+$  and  $\text{Sr}^{2+}$ , other elements such as  $\text{Cd}^{2+}$  and  $\text{Pb}^{2+}$  [23], and radionuclides such as  $^{152}\text{Eu}$ ,  $^{60}\text{Co}$ ,  $^{59}\text{Fe}$  and isotopes of Am and Pu have also been successfully immobilised in AAMs [24–26].

Concerning the use of AAMs for RAW immobilisation, most literature covers AAMs based on commercial recipes, MK, fly ash (FA), ground granulated blast furnace slag (GGBFS) or combinations thereof. Despite the large body of research and the promising immobilisation results, a systematic study of the influence of the precursor composition on the immobilisation capacities for  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  is lacking. According to *Aly et al.* (2008) [12], MK-based AAMs show optimal leach resistance at Si/Al ratios higher than 2. They reported a sharp decrease in the  $\text{Cs}^+$  release when the Si/Al ratio increased from 1.5 to 2 followed by a gradual increase at Si/Al ratios higher than 3, reaching the lowest value at Si/Al ratio of 2. For  $\text{Sr}^{2+}$ , the lowest release was obtained at a Si/Al ratio of 1.5, increasing gradually with increasing Si/Al ratio [12].

Almost all concerning literature describes AAMs made from industrial residues, making it difficult to exclude effects of trace elements in the precursor on the immobilisation capacities. Also, the variety in precursor origin and composition in most studies make it difficult to generalize the drawn conclusions, since the immobilisation performance is very dependent on the design parameters. In addition, there exists a wide variety of alkali-activators used, most often consisting of highly-alkaline activating solutions and often containing sodium silicates.

According to the IAEA [27], the lack of standards for precursors, experience of process optimization, and demonstration of long-term stability limit their use in RAW immobilisation, despite the reported favourable experiences using AAMs. They stated that novel materials need a better benchmarking, and emphasised that it is also important to realise that existing test methods do not always give comparable results with different classes of materials [27]. Therefore, the effect of precursor composition on the immobilisation of  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  in AAMs is studied in this work, by developing synthetic Ca-Si-Al slag precursors with different compositions from laboratory reagents, yielding Si/Al and Ca/(Si+Al) molar ratios of 0.95 – 5.1 and 0.42 – 1.0 respectively. In this way, immobilisation is studied excluding possible effects of trace elements in the mixture. The present results can be further used as a guideline for choosing industrial residues with a proper composition or for using proper mixing ratios.

## **2 Materials and methods**

### *2.1 Ca-Si-Al slag synthesis*

Ca-Si-Al slags were synthesised from analytical grade laboratory reagents  $\text{Al}_2\text{O}_3$ ,  $\text{SiO}_2$  and  $\text{CaCO}_3$  (all Sigma-Aldrich, > 99 % pure). The studied compositions (**Table 1**) were chosen to broadly resemble GGBFS and to be fully liquid at 1550 °C (see **Figure 1**). The  $\text{CaCO}_3$  was first calcined in a muffle furnace at 1050 °C overnight to expel  $\text{CO}_2$ . For each composition, the exact mass of  $\text{CaCO}_3$  necessary for achieving the stoichiometric amount of CaO was weighed and inserted into the muffle furnace.

Immediately after cooling, the mass of the obtained CaO was determined to verify the complete decarbonation. The resulting CaO was then mixed with weighed amounts of Al<sub>2</sub>O<sub>3</sub> and SiO<sub>2</sub> for two hours in a Turbula T2C mixer for homogenization. The mixtures were placed in a platinum crucible and inserted into a bottom loading furnace (AGNI ELT 160-02) at 1630 °C. A higher temperature was applied to account for possible differences in temperature between the location of the crucible and the thermocouple of the furnace, to ensure that the sample would melt completely. After an isothermal period of 2.5 h, the melt was quenched by pouring in water at room temperature. The cooled slag was then dried at 110 °C to constant weight before being crushed and milled in a Retsch disk mill RS200 at 1000 rpm for 60 s.

Homogeneity of the finely milled slag was confirmed by X-ray diffraction spectroscopy (XRD). The measurements were performed with a Bruker D8 diffractometer. This theta-theta diffractometer is equipped with a Göbel mirror (line focus, Cu k<sub>α</sub> radiation). The X-rays are detected with a 1D lynxeye detector.

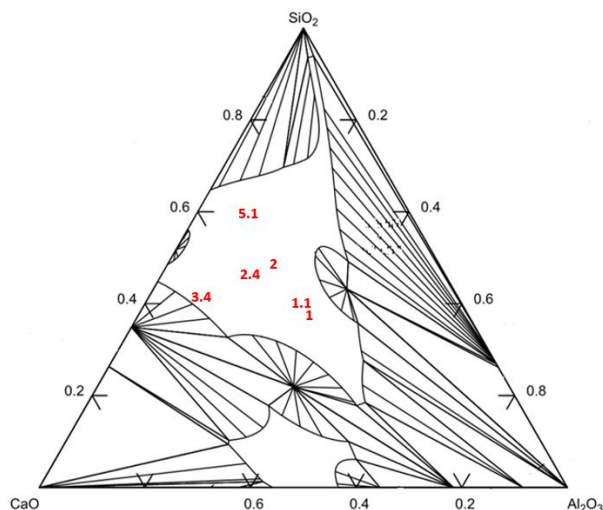
The specific surface area of the resulting powders was measured in threefold by use of Blaine method. The procedures described in the standard EN 196-6 [28] were followed as closely as possible and the measurements were performed against a reference cement sample. It is, however, important to note that the Blaine method is designed for cements and that results may deviate when using other types of materials.

**Table 1:** Designed compositions of synthetic slags (wt fraction) and the initial Si/Al and Ca/(Si+Al) molar ratios. The labelling of the samples is based on the initial Si/Al ratio.

	SiO <sub>2</sub> wt fraction	Al <sub>2</sub> O <sub>3</sub> wt fraction	CaO wt fraction	Si/Al mol/mol	Ca/(Si+Al) mol/mol
S_1	0.37	0.33	0.30	0.95	0.42
S_1.1	0.40	0.30	0.30	1.1	0.43
S_2	0.49	0.21	0.30	2.0	0.44
S_2.4	0.47	0.17	0.36	2.4	0.59

S_3.4	0.40	0.10	0.50	3.4	1.0
S_3.4b*	0.40	0.10	0.50	3.4	1.0
S_5.1	0.60	0.10	0.30	5.1	0.45

\*This composition, randomly chosen, has been made as a replicate to check the reproducibility of the experimental design



**Figure 1:** Phase diagram at 1550 °C. The designed compositions are all within the liquid (white) area.

## 2.2 AAM elaboration

AAM pastes were prepared by mixing the powdered slag precursors with a 2 M NaOH solution (prepared from NaOH pellets (Fischer Scientific, 98.44 % pure) and type II distilled water) using a laboratory mixer and maintaining a liquid to solid ratio (L/S) of 0.30. These parameters were chosen based on our earlier study [29] and adjusted for optimal workability and setting time. At this molarity and L/S ratio, the amount of Na<sup>+</sup> added is 1 wt% for each sample. Cs<sup>+</sup> and Sr<sup>2+</sup> were added as nitrates (CsNO<sub>3</sub>, Alfa Aesar 99.8%; Sr(NO<sub>3</sub>)<sub>2</sub>, Emsure 99.0%) to account for 1 wt% and 0.1 wt% respectively of the final AAM-mass (solid precursor + activating solution). A lower wt% of Sr<sup>2+</sup> was chosen to avoid significant interference with the polymerisation kinetics, as reported in our earlier studies [29,30]. The resulting mixtures were poured into plastic (polymethylmethacrylate, PMMA) 25 x 25 x 20 mm<sup>3</sup> moulds. The moulds were manually tapped during 60 seconds to remove air bubbles before being

sealed with a PMMA cap. These pastes were then allowed to cure for 28 days at  $23 \pm 1$  °C. Each composition was made in threefold for the leaching experiments.

### 2.3 Leaching of introduced and structural elements

The release of introduced caesium and strontium, and of the structural elements silicon, aluminium, calcium and sodium was measured using a semi-dynamic diffusion test described in our earlier study [29] and based on the standards ASTM C1220-98 [31] and CEN/TS 15863:2015 [32]. The samples were demoulded, cleaned with a dry brush and measured for dimensions and weight before being submerged in 400 ml of pre-heated Milli-Q water (90 °C, polypropylene bottle and sample holder). Before and after the eluate was refreshed, the mass of the closed container was measured to determine water loss through evaporation. In all cases, the loss of mass through evaporation was lower than 2 %, which is in line with the standard ASTM C1220-98 [31]. At each sampling time (1 h, 24 h, 7 d, 28 d), 10.0 ml of the eluate was filtered over a 0.2 µm syringe filter and acidified immediately after sampling to a concentration of 2 % HNO<sub>3</sub> (MERCK Suprapur 65 %). The concentrations of water-soluble Sr<sup>2+</sup>, Si<sup>4+</sup>, Al<sup>3+</sup>, Ca<sup>2+</sup>, and Na<sup>+</sup> were measured by ICP-OES (Perkin Elmer type Optima 8300) in axial mode. The concentration of water-soluble Cs<sup>+</sup> was measured by ICP-MS (Perkin Elmer NexION 350S). At each sampling time, the eluate was also measured for pH (calibrated electrode HI1043B, Hanna Instruments) and conductivity (Schott Geräte CG 858, calibrated with 0.1 M KCl).

The release  $r$  (mg/m<sup>2</sup>) of element  $i$  at leaching interval  $n$  is calculated as:

$$r_{i,n} = \frac{(C_{i,n} - B_{i,n}) \cdot V}{A_s} \quad (1)$$

With

$C_{i,n}$  = concentration of element  $i$  in the filtered aliquot of leaching interval  $n$  (mg/ml)

$B_{i,n}$  = concentration of element  $i$  in the filtered blanc aliquot of leaching interval  $n$  (mg/ml)



146  $V$  = initial volume of eluate in the bottle containing the sample AAM (ml)

147  $A_s$  = geometric surface area of the sample AAM (m<sup>2</sup>)

148 The cumulative release  $R$  (mg/m<sup>2</sup>) of each constituent is calculated as:

$$R_i = \sum_0^n r_{i,n} \quad (2)$$

149 The normalized leach rate  $LR$  (mg/(m<sup>2</sup>.s)) of element  $i$  at leaching interval  $n$  is calculated as:

$$LR_{i,n} = \frac{r_{i,n}}{\Delta t_n \cdot f_i} \quad (3)$$

150 with  $\Delta t_n$  the time of leaching interval  $n$  (in seconds) and  $f_i$  the fraction of element  $i$  in the sample, as

151 to account for possible differences in waste loadings. The total release of element  $i$  (%  $release_i$ ) and

152 the percentage of wash-off in the first leaching interval (%  $WO_i$ ) are defined as:

$$\% release_i = \frac{R_{i,28d} \cdot A_s}{m_s \cdot f_i} \cdot 100 \% \quad (4)$$

$$\% WO_i = \frac{R_{i,1h}}{R_{i,28d}} \cdot 100 \% \quad (5)$$

153 with  $m_s$  the mass of the sample (mg) after demoulding.

#### 154 2.4 Effect of leaching temperature and specific surface area on immobilisation performance

155 To confirm the observed relation between immobilisation capacity and the AAM design ratios, the

156 immobilisation capacity of selected compositions has been tested under varying conditions. Samples

157 of compositions AAM\_1, AAM\_1.1, AAM\_2 and AAM\_5.1 were leached at a lower temperature of 20

158  $\pm 1$  °C for 7 days. The specific surface area of these samples was measured. The Brunauer Emmett

159 Teller (BET) surface area, was measured for these samples by continuous flow method using 0.3

160 ml/min of nitrogen gas (Tristar 3000).

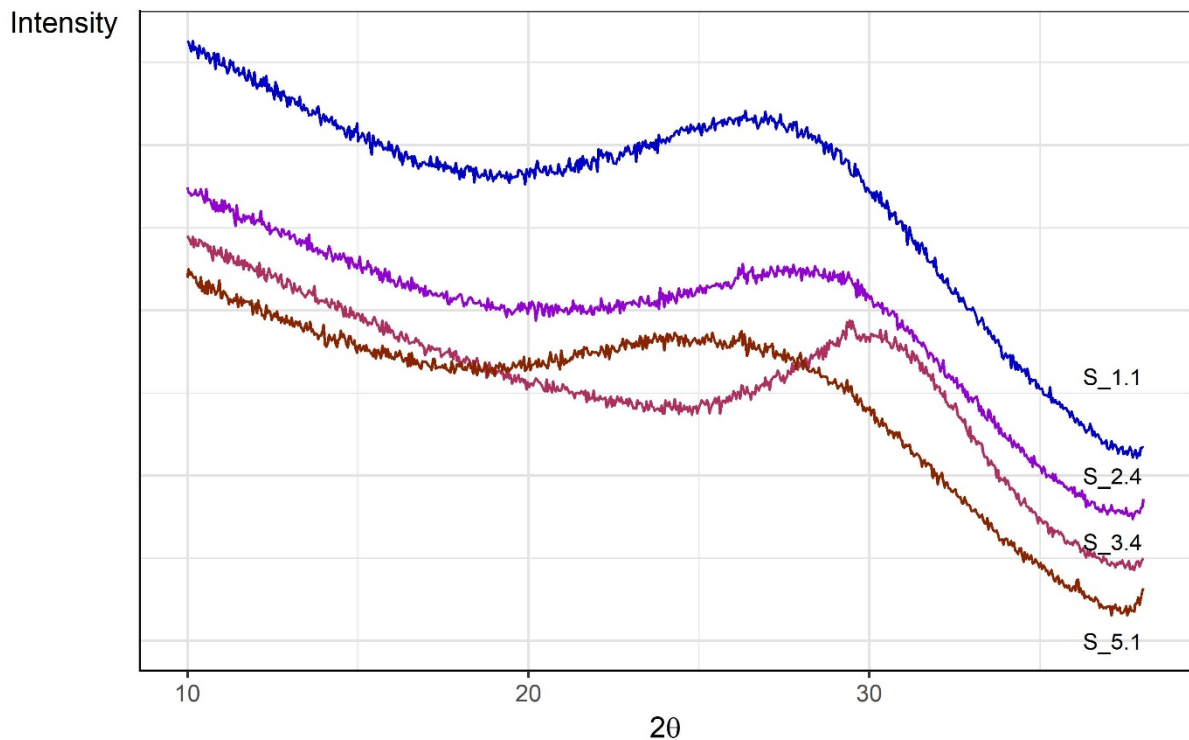
### 2.5 Effect of slag fineness on immobilisation performance

The effect of slag fineness on the immobilisation performance is studied by further milling slag precursors S\_1 and S\_2 for an additional 30 s. From these finer slags, additional samples of composition AAM\_1 and AAM\_2 were prepared for leaching during 7 d at  $20 \pm 1$  °C.

## 3 Results and discussion

### 3.1 Homogeneity of the slag

All mixtures were completely molten during the isothermal period in the bottom loading furnace. Water-quenching of the melt gave rise to a clear transparent glass for all mixtures. XRD patterns of selected slag samples S\_1.1, S\_2.4, S\_3.4 and S\_5.1 are presented in **Figure 2**. No crystalline phases were detected in any of the measured slags, indicating homogeneity without crystalline inclusions.

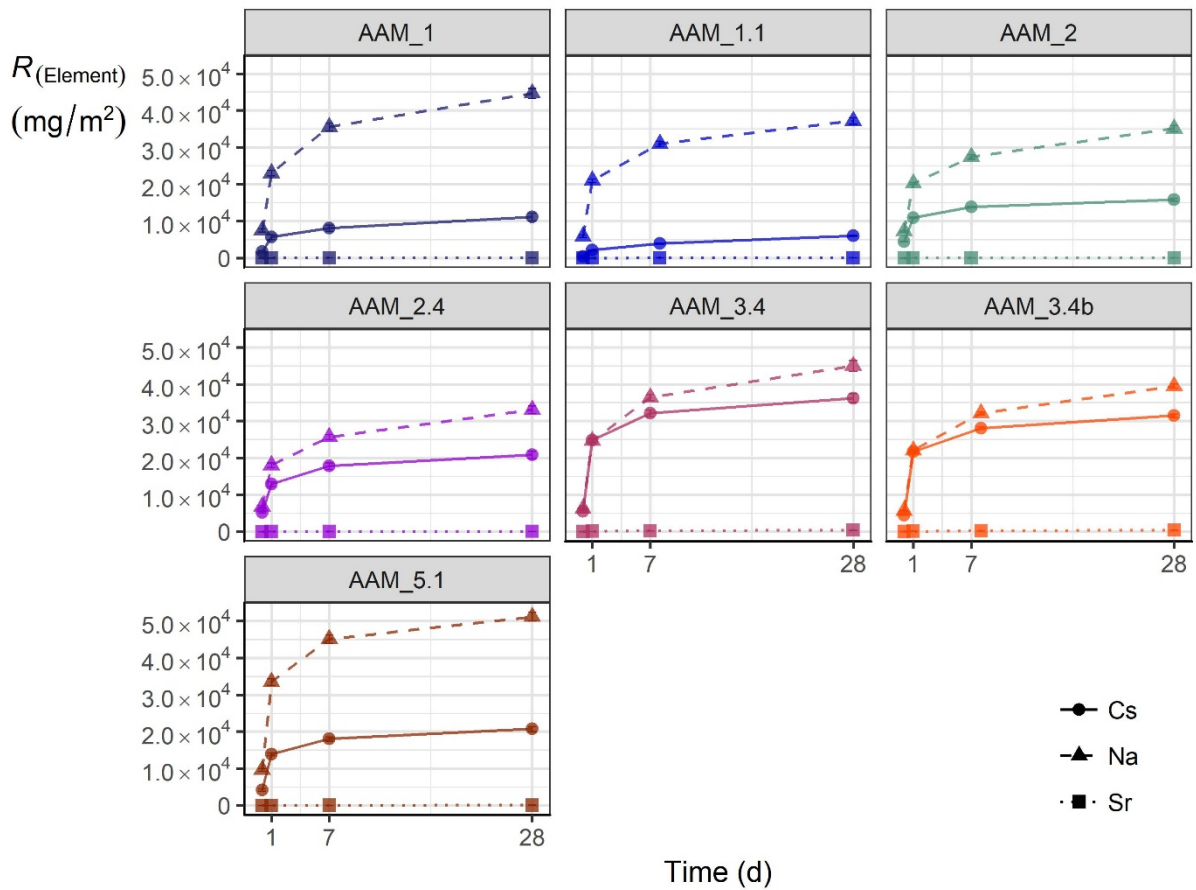


**Figure 2:** XRD patterns of the finely milled slags S\_1.1, S\_2.4, S\_3.4 and S\_5.1.

### 3.2 Immobilisation of $\text{Cs}^+$ , $\text{Sr}^{2+}$ and $\text{Na}^+$

**Figure 3** shows the cumulative release for  $\text{Cs}^+$ ,  $\text{Sr}^{2+}$  and  $\text{Na}^+$  in function of the leaching time. The % release is summarized in **Table 2**. The highest  $\text{Na}^+$  leaching is measured in AAM\_5.1, which is also the sample with the highest Si/Al ratio. AAM\_1.1 shows the best  $\text{Cs}^+$  immobilisation, releasing only  $7.8 \pm 0.3$  % of the introduced  $\text{Cs}^+$ , which is almost twice as good as the second best (AAM\_1). In our earlier study [29], GGBFS-based AAMs activated with 6 M NaOH were leached for 7 days under the same conditions. The composition of the GGBFS closely resembles that of S\_3.4 (excluding the contribution of  $\text{MgO}$ ,  $\text{SO}_3$  and other trace elements). With a 1 wt%  $\text{Cs}^+$  loading, the GGBFS-AAM leached 66 % of the introduced  $\text{Cs}^+$  [29]. This is much higher than the  $\text{Cs}^+$  release observed in AAM\_3.4 and AAM\_3.4b which could be due to e.g. the differences in activating solution molarity or the presence of magnesium and other elements. Among the compositions tested in this study, AAM\_3.4 performs worst regarding both  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  immobilisation indicating that the composition of GGBFS requires optimisation regarding immobilisation purposes.

The  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  normalized leach rates are given in **Table 3**. The effect of initial wash-off ( $\%WO_{\text{Cs}}$ ) seems to be the least pronounced for AAM\_1.1 (see **Table 3**) with a percentage released in the first hour of leaching of 7 % of the total amount leached. Also for  $\text{Sr}^{2+}$ , AAM\_1.1 clearly shows the best immobilisation, releasing only  $0.50 \pm 0.04$  % of the introduced  $\text{Sr}^{2+}$ , which is about 50 % better than the second best (AAM\_2). The overall percentage of wash-off ( $\%WO_{\text{Sr}}$ , see **Table 3**) is lower for  $\text{Sr}^{2+}$  than for  $\text{Cs}^+$  indicating a slower release from the sample surface.



**Figure 3:** Cumulative release of  $\text{Cs}^+$ ,  $\text{Na}^+$  and  $\text{Sr}^{2+}$  during a 28-d leaching test at 90 °C.

**Table 2:** Percentage of introduced  $\text{Cs}^+$ ,  $\text{Sr}^{2+}$  and  $\text{Na}^+$  that has been released by leaching for 28 d at 90 °C. Uncertainties are calculated as standard deviations from 3 samples per composition.

$\% \text{ release}_i$	$\text{Cs}^+$	$\text{Sr}^{2+}$	$\text{Na}^+$
AAM_1	14 ± 2	1.11 ± 0.07	58 ± 2
AAM_1.1	7.8 ± 0.3	0.5 ± 0.04	49 ± 2
AAM_2	20.1 ± 0.5	0.74 ± 0.3	46 ± 1
AAM_2.4	40 ± 2	1.4 ± 0.2	65 ± 2
AAM_3.4	46 ± 2	4.9 ± 0.5	59 ± 2
AAM_3.4b	40.9 ± 0.7	5 ± 0.4	53 ± 1
AAM_5.1	27.8 ± 0.9	0.9 ± 0.1	71 ± 2

**Table 3:** Average leach rates (mg/(m<sup>2</sup>.s)) of Cs<sup>+</sup> and Sr<sup>2+</sup> during a 28-d leaching period at 90 °C. The mean value calculated per sample is weighted for the time of the respective leaching interval. %WO<sub>i</sub> (wash-off) is the percentage of the total released amount leached in the first hour of the test.

	Leaching time (h)	AAM_1	AAM_1.1*	AAM_2	AAM_2.4	AAM_3.4	AAM_3.4b*	AAM_5.1
<b>LR<sub>Cs</sub></b>	1	49	12	120	150	150	120	120
	24	4.7	2.0	7.8	9.3	23	21	12
	168/192*	0.47	0.30	0.55	0.94	1.4	1.1	0.80
	672	0.13	0.09	0.09	0.13	0.18	0.14	0.12
	<b>Mean</b>	0.43	0.23	0.64	0.83	1.5	1.3	0.83
<b>%WO<sub>Cs</sub></b>		16	7	28	25	15	14	20
<b>LR<sub>Sr</sub></b>	1	0.68	0.53	0.39	1.5	10	12	0.77
	24	0.14	0.070	0.24	0.36	0.94	1.1	0.20
	168/192*	0.047	0.017	0.036	0.035	0.27	0.22	0.033
	672	0.022	0.0089	0.0079	0.0088	0.054	0.049	0.012
	<b>Mean</b>	0.032	0.014	0.023	0.029	0.15	0.15	0.024
<b>%WO<sub>Sr</sub></b>		3	5	2	8	10	11	4

The overall leaching behaviour as seen in **Figure 3** is comparable for all samples and comprises a decreasing leaching rate with increasing leaching time. E.g. *LR<sub>Cs</sub>* for AAM\_1 is 49 mg/(m<sup>2</sup>.s) in the first hour of leaching, decreases with a factor 10 for each following step (24 h, 7 d) and levels off in the final interval (see **Table 3**). For both Cs<sup>+</sup> and Sr<sup>2+</sup>, the leach rate for all samples is highest in the first hour of leaching. This behaviour is typical for materials with an initial surface wash-off, which is a process that occurs often in this type of tank test for monolithic materials and comprises the fast dissolution of soluble salts from the surface of the monolith [33]. In addition to surface wash-off, diffusion of the element of interest through the sample and eventual depletion of the element from the sample are important processes governing the leaching behaviour.

Diffusion-controlled release from a monolithic waste form is related to the surface area of the waste form and the time of exposure [33]. In semi-dynamic tank leaching tests with a monolithic sample, a one-dimensional semi-infinite diffusion model, based on Fick's second law, is often assumed [34,35].

214 In this model, mass transfer is assumed to take place in response to concentration gradients in the  
215 pore water solution of the structure [35]. When Fickian diffusion is considered as the dominant  
216 release mechanism, the mass release should be proportional to the square root of the release time  
217 ( $R \sim t^{0.5}$ ); this results in a straight line with a slope of 0.5 when the logarithm of the cumulative  
218 release is plotted against the logarithm of the release time [35]. Initial surface wash-off causes a  
219 higher release in the first stage of leaching, while depletion leads to a levelling-off of the cumulative  
220 release curve [33].

221 **Figure 4** shows the cumulative **caesium and strontium** release of a selected subset of samples (the  
222 remaining samples show similar behaviour) plotted against the release time on a double logarithmic  
223 scale. None of the samples closely follow the 0.5 slope. Since an initial wash-off and depletion of  $\text{Cs}^+$   
224 is clear from **Table 2** and **Table 3**, the results from the leaching test can be divided into the intervals  
225 [1 h ; 24 h] and [24 h ; 28 d] as shown in **Figure 4a** for  $\text{Cs}^+$  and **Figure 4b** for  $\text{Sr}^{2+}$ .

226 For **caesium**, it is clear from **Figure 4a** that the sample with limited wash-off (AAM\_1.1, as seen in  
227 **Table 3**) has a slope close to 0.5 in the interval [1 h ; 24 h] indicating possible diffusion-controlled  
228 release. AAM\_2 shows a slope of 0.28 in this first interval, indicating a significant wash-off (high  
229 concentration in the first hour of leaching).

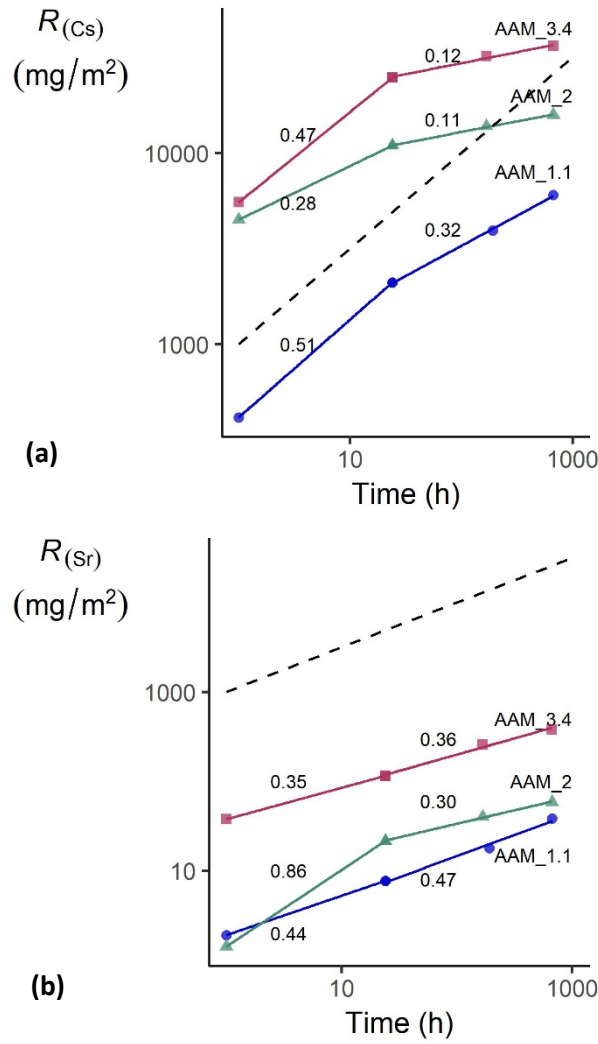
230 In the interval [24 h ; 28 d], the regression lines flatten for all samples (slope < 0.5) indicating signs of  
231 depletion. Since depletion is only assumed to occur when the total release is higher than 20 % [35],  
232 not all samples have actually been significantly depleted. **Table 2** shows that the release of  $\text{Cs}^+$  from  
233 the AAMs is between 46 and 7 %. The fact that depletion-like behaviour occurs even in samples with  
234 a low release indicates a possible distribution of the present  $\text{Cs}^+$  into an easily-leachable fraction and  
235 a strongly-bound fraction. The occurrence of the wash-off and the depletion effects can then be  
236 contributed to the easily-leachable fraction. The levelling-off of the regression curve could thus be  
237 caused by the depletion of the readily available  $\text{Cs}^+$ , while the remaining fraction is more strongly  
238 bound in the AAM structure. The leaching behaviour of  $\text{Cs}^+$  can thus be summarized as a combination

of initial wash-off, diffusion, and depletion of an easily-released fraction. The lower the Si/Al and Ca/(Si+Al) ratio, the smaller this easily-leachable fraction (as discussed further).

For **strontium**, the leaching behaviour in most samples does not seem to be dependent on the leaching interval as seen in **Figure 4b**. The overall slopes of the regression curves are smaller than 0.5, indicating depletion. Since the total amount of leached  $\text{Sr}^{2+}$  is small for all samples (< 5 %, see **Table 2**), it seems reasonable that  $\text{Sr}^{2+}$  leaches only from the sample surface, slowly depleting while the bulk of the  $\text{Sr}^{2+}$  remains encapsulated in the sample, not available for leaching.

The amount of **sodium** leached does not correspond with the amount of  $\text{Cs}^+$  leached (see **Table 2**), as would be expected since  $\text{Cs}^+$  is known to act as a charge-balancing ion, replacing  $\text{Na}^+$  in the framework [13,15]. This indicates that  $\text{Cs}^+$  and  $\text{Na}^+$  immobilisation is not completely similar, and shows that  $\text{Cs}^+$  is retained better than  $\text{Na}^+$  (since  $\text{Na}^+$  release is higher and both were introduced as 1 wt%). This is consistent with the findings of *Kuenzel et al. (2015)* [15], who reported that the reaction between  $\text{Cs}^+$  and  $\text{Al}(\text{OH})_4^-$  is favoured over that of  $\text{Na}^+$  because of the lower charge density of  $\text{Cs}^+$ . In addition, the difference in immobilisation between  $\text{Cs}^+$  and  $\text{Na}^+$  is dependent on the AAM composition, since from **Table 2** it can be seen that e.g. AAM\_2 releases the least  $\text{Na}^+$  (46 %) while releasing 20 %  $\text{Cs}^+$ ; in contrast, AAM\_1 leaches less  $\text{Cs}^+$  (14 %) and more  $\text{Na}^+$  (58 %). This could indicate a difference in hydrate phases formed depending on the AAM composition. The findings of *Kuenzel et al. (2015)* [15] were based on MK-AAMs, resulting in an amorphous sodium aluminosilicate hydrate (N-A-S-H) as the main binder phase.

A difference in the amount of N-A-S-H formed (as compared to calcium sodium aluminosilicate hydrate (C-(N)-A-S-H)) could be the cause of the difference in leaching behaviour of  $\text{Na}^+$  as compared to  $\text{Cs}^+$ . Based on the initial composition of the slags and the use of a NaOH activator, the AAMs are expected to consist mainly of C-(N)-A-S-H gel, N-A-S-H gel (due to high Al content), strätlingite, and some zeolitic phases [36–38]. For the low Si/Al samples AAM\_1 and AAM\_1.1, the ratio of leached  $\text{Na}^+/\text{Cs}^+$  is much higher than for the high Si/Al samples (see **Table 2**).

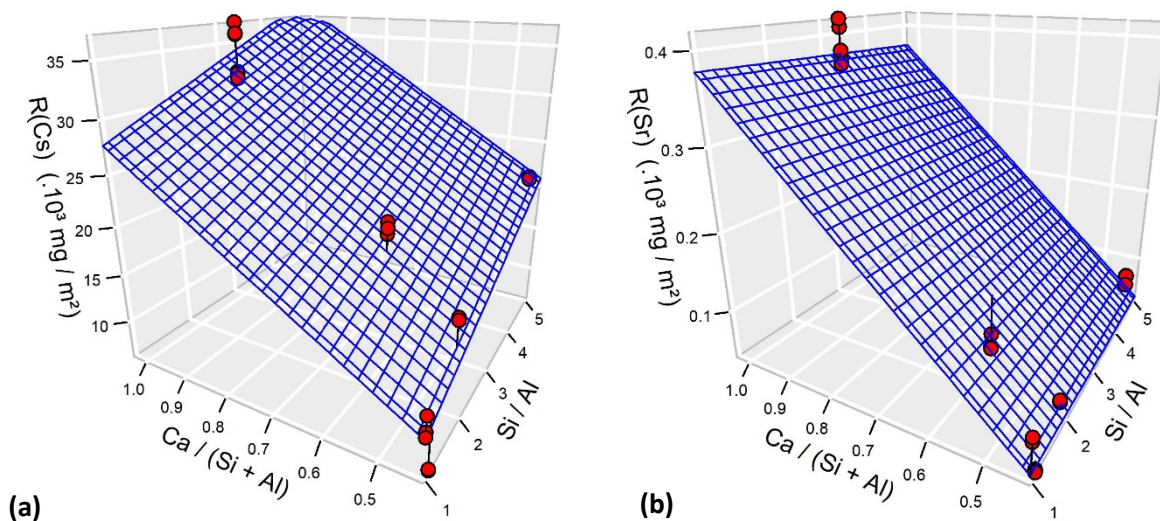


**Figure 4: (a)**  $R_{Cs}$ , dividing the leaching time into two intervals [1 h ; 24 h] and [24 h ; 28 d] and **(b)**  $R_{Sr}$ , dividing the leaching time into two intervals.  $R^2$ -values are all  $> 0.97$  for **(a)** and **(b)**. The dashed line represents the slope of 0.5 from a diffusion-based release. The slopes are indicated on the graph next to the regression lines.

When linking the immobilisation capacity for  $Cs^+$  and  $Sr^{2+}$  with the precursor composition, an initial Si/Al ratio of about 1.1 (**Table 2**) seems to be best. **Figure 5a** shows the cumulative 28-d release of  $Cs^+$  in function of the Si/Al and Ca/(Si+Al) ratios of the precursor slags. For the studied compositions,  $Cs^+$  is immobilised better in AAMs with lower Si/Al ratios and lower Ca/(Si+Al) ratios.



**Figure 5b** shows the cumulative 28-d release of  $\text{Sr}^{2+}$  in function of the Si/Al and Ca/(Si+Al) ratios of the precursor slags. For the studied compositions, the immobilisation of  $\text{Sr}^{2+}$  is dependent on the Ca/(Si+Al) ratio, but not on the Si/Al ratio. This indicates a competition between  $\text{Ca}^{2+}$  and  $\text{Sr}^{2+}$  for incorporation into the AAM structure. The independence of strontium leaching to the Si/Al ratio is in contrast with the results of the study of *Aly, et al.* (2008) [12], where  $\text{Sr}^{2+}$  release increased in samples with an increasing Si/Al ratio from 1.5 to 4. This could be due to the fact that the samples studied by *Aly, et al.* (2008) [12] were low in calcium, indicating the possible differences in leaching behaviour in function of the type of AAMs.



**Figure 5:** The cumulative 28-d release of  $\text{Cs}^+$  **(a)** and  $\text{Sr}^{2+}$  **(b)** ( $10^3 \text{ mg/m}^2$ ) in function of the Si/Al and Ca/(Si+Al) ratios of the precursor slags. The regression planes are a result of multiple linear regressions with  $R^2$ -values  $> 0.93$ .

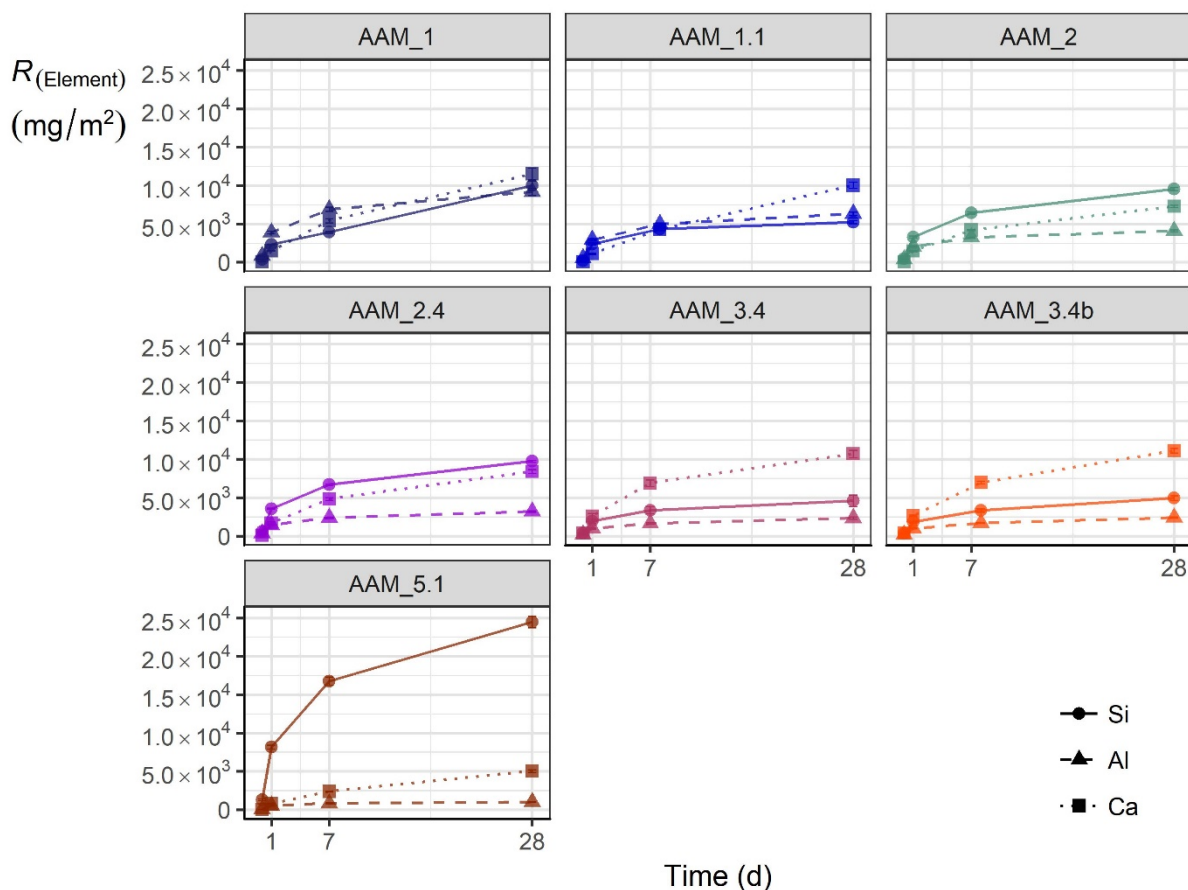
### 3.3 Release of structural elements

The  $\text{Ca}^{2+}$  release of AAM\_1, AAM\_1.1, AAM\_3.4 and AAM\_3.4b are similar, while S\_1 and S\_1.1 have a CaO content of only 30 % and S\_3.4 and S\_3.4b have an initial CaO content of 50 %. Also, the  $\text{Ca}^{2+}$  release decreases with increasing Si/Al ratio reaching a value of  $7300 \pm 200 \text{ mg/m}^2$  for AAM\_2 and  $5000 \pm 200 \text{ mg/m}^2$  for AAM\_5.1. This higher  $\text{Ca}^{2+}$  release at lower Si/Al ratios explains why AAM\_1, AAM\_1.1, AAM\_3.4 and AAM\_3.4b show a similar  $\text{Ca}^{2+}$  release while having a lower calcium content.

290 This behaviour of calcium leaching could be an indication of less C-(N)-A-S-H formation at lower Si/Al  
291 ratios since the formation of this phase would better immobilise  $\text{Ca}^{2+}$  into the structure. An increased  
292 Al content (and thus lower Si/Al ratio) promotes the formation of N-A-S-H in addition to C-(N)-A-S-H,  
293 while an increased Ca content impedes the formation of N-A-S-H [38]. Higher Si/Al ratios will thus  
294 give rise to more C-(N)-A-S-H formation.

295 The highest **silicon** release is observed in AAM\_5.1 ( $\approx 24\,000\text{ mg/m}^2$ ), while AAM\_3.4, AAM\_3.4b,  
296 and AAM\_1.1 show the lowest silicon release ( $\approx 5000\text{ mg/m}^2$ ). AAM\_2.4, AAM\_2, and AAM\_1 all  
297 show a 28-d cumulative silicon release around  $10\,000\text{ mg/m}^2$ . The lower silicon leaching of AAM\_3.4  
298 and AAM\_3.4b as compared to AAM\_2.4, AAM\_2, and AAM\_1 (while having similar initial  $\text{SiO}_2$   
299 contents) indicates that a higher calcium content increases the immobilisation of silicon, which again  
300 indicates the formation of C-(N)-A-S-H.

301 Regarding **aluminium**, the release follows the Si/Al ratio, with AAM\_5.1 showing the lowest  
302 aluminium release and increasing with decreasing Si/Al. For AAM\_1, the amount of silicon and  
303 aluminium released is almost equal (AAM\_1:  $R_{\text{Si}} = 10000 \pm 600\text{ mg/m}^2$ ,  $R_{\text{Al}} = 9200 \pm 500\text{ mg/m}^2$ ),  
304 indicating congruent dissolution.



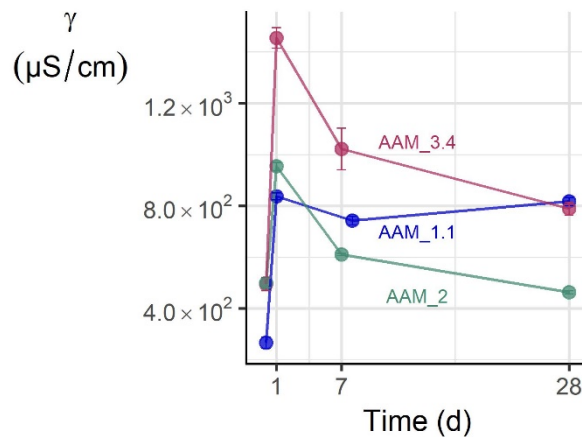
**Figure 6:** Cumulative release of silicon, aluminium and calcium during a 28-d leaching test at 90 °C.

### 3.4 pH and conductivity

The measured pH of the eluates was similar for all samples. After 1 h of leaching the average pH over all samples was  $10.7 \pm 0.3$ . After 24 h, the pH of the eluates increased to  $11.2 \pm 0.3$ . After 28 d, the pH-values were  $11.3 \pm 0.6$ . The conductivity of selected eluates is given in **Figure 7**.

AAM\_5.1, AAM\_3.4, AAM\_3.4b, AAM\_2.4 and AAM\_2 show a high peak in conductivity at 24 h (only AAM\_2 and AAM\_3.4 shown in **Figure 7**), while decreasing at later sampling times. This high early peak in ionic conductivity followed by a gradual decrease indicates a more profound early wash-off and subsequent depletion, which is consistent with the results seen for  $\text{Cs}^+$  in **Figure 4a**. This effect is not so pronounced for AAM\_1.1, which shows a slighter decrease in conductivity at the 7 d sampling time. Regarding the validity of the experimental design, the duplicates AAM\_3.4 and AAM\_3.4b show

very similar results in all measured leaching aspects, confirming that the slag development, the AAM development, and the leaching tests are very well reproducible.



**Figure 7:** Conductivity values (μS/cm) of AAM\_1.1, AAM\_2 and AAM\_3.4 at each sampling time.

### 3.5 Effect of leaching temperature on immobilisation capacity

**Table 4** and **Table 5** show that the leaching temperature has a profound effect on the release of all constituents. However, this effect is not the same for all samples. AAM\_1 exhibits significantly less release at 20 °C than at 90 °C for Cs<sup>+</sup>, Sr<sup>2+</sup> and Na<sup>+</sup>, while AAM\_5.1 exhibits less release for Sr<sup>2+</sup> and Na<sup>+</sup> but not for Cs<sup>+</sup>. In contrast, AAM\_1.1 has a significantly higher release at 20 °C as compared to 90 °C for all constituents, while AAM\_2 has a higher release for Cs<sup>+</sup> and Na<sup>+</sup> at 20 °C and a similar release for Sr<sup>2+</sup>. Although all samples were completely set after 28 days of curing, it appears that the high temperature (90 °C) of the leaching environment influenced the curing of AAM\_1.1 and AAM\_2 which significantly improved their immobilisation potential. This does not seem to be the case for AAM\_1 and AAM\_5.1.

**Table 4:** Slag Blaine values, % *release* and BET values for samples leached for 7 d at 20 °C. The % *release* values are given as individual measurements since only one or two samples were tested per composition.

	Slag Blaine (m <sup>2</sup> /kg)			% release 7 d, 20 °C			BET (m <sup>2</sup> /g)		
Sample				Cs <sup>+</sup>	Sr <sup>2+</sup>	Na <sup>+</sup>			
AAM_1	110	±	20	2.97; 3.06	0.13; 0.22	31.52; 31.77	10.7	±	0.1
AAM_1.1	200	±	20	11.22	4.02	60.21	14.8	±	0.1
AAM_2	140	±	10	26.56; 27.94	0.27; 0.49	41.29; 42.76	3.8	±	0.1
AAM_5.1	310	±	10	22.45; 22.71	0.20; 0.22	53.88; 55.21	37.5	±	0.1

**Table 5:** Percentages of Cs<sup>+</sup>, Sr<sup>2+</sup> and Na<sup>+</sup> released after 7 d leaching at 90 °C.

	% release 7 d, 90 °C								
Sample	Cs <sup>+</sup>			Sr <sup>2+</sup>			Na <sup>+</sup>		
AAM_1	10	±	1	0.48	±	0.05	46	±	2
AAM_1.1	5.1	±	0.2	0.23	±	0.03	41	±	1
AAM_2	17.5	±	0.3	0.51	±	0.2	36	±	1
AAM_5.1	24.2	±	0.7	0.49	±	0.06	62	±	2

### 3.6 Effect of specific surface area on immobilisation capacity

The BET specific surface area (before leaching) of the samples used for leaching at 20 °C is given in **Table 4**. The BET specific surface area is lowest for AAM\_2, while AAM\_5.1 exhibits the highest BET area. The specific surface areas of AAM\_1 and AAM\_1.1 are comparable. AAM\_2 releases more Cs<sup>+</sup> and Sr<sup>2+</sup> than AAM\_5.1 at 20 °C, although having a much lower BET value. From the tested samples, no clear correlation could be established between the BET values and the immobilisation capacities.

### 3.7 Effect of slag fineness on immobilisation capacity

The remainder of slag precursors S\_1 and S\_2 were further milled for an additional 30 s. The higher Blaine values (HB) of these slags are given in **Table 6**. From these finer slags, additional samples of

composition AAM\_1 and AAM\_2 were prepared for leaching during 7 d at  $20 \pm 1$  °C. The percentages of  $\text{Cs}^+$ ,  $\text{Sr}^{2+}$  and  $\text{Na}^+$  leached under these new leaching conditions are given in **Table 6**.

Increasing the slag fineness of S\_2 to a comparable value of that of S\_5.1 (see **Table 4**) reduces the  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  release of AAM\_2 by a factor 2, increasing its immobilisation capacity beyond that of AAM\_5.1. AAM\_1 shows the greatest immobilisation potential for all constituents at 20 °C, despite having the smallest Blaine specific surface area of the slag. Increasing the slag fineness of S\_1 and S\_2 demonstrates its significant effect on the immobilisation potential. The increased Blaine value of 220  $\text{m}^2/\text{kg}$  for S\_1 (which is now comparable to that of S\_1.1) further increases the immobilisation potential for all constituents. The same effect is observed for AAM\_2. Increasing the slag fineness leads to a larger fraction of small slag particles that can be readily dissolved to form hydrate phases. This, in turn, raises the need for more charge-balancing ions, thus increasing the incorporation potential.

The results of the effect of leaching temperature, and the differences in specific surface area and slag fineness support the earlier established relationship between the immobilisation potential and design parameters Si/Al and Ca/(Si+Al). Leaching at 20 °C strengthens the conclusion that low Si/Al and Ca/(Si+Al) ratios provide a higher immobilisation potential since AAM\_1 now exhibits the best immobilisation potential (see **Table 5** and **Table 6**). Under the experimental conditions, a Si/Al ratio of 1 thus seems optimal for immobilising  $\text{Cs}^+$  and  $\text{Sr}^{2+}$ .

**Table 6:** Higher Blaine values (HB) after additional milling and % *release* after 7 d leaching at 20 °C of AAM\_1 and AAM\_2 prepared with HB-slag.

Sample	Slag Blaine HB ( $\text{m}^2/\text{kg}$ )	% <i>release</i> 7 d, 20 °C		
		$\text{Cs}^+$	$\text{Sr}^{2+}$	$\text{Na}^+$
AAM_1	220 ± 10	2.38	0.05	22.03
AAM_2	380 ± 10	12.79	0.18	31.48

370

#### 371 **4 Conclusion**

372 The effect of AAM composition regarding Si/Al and Ca/(Si+Al) ratios on the immobilisation capacity of  
373 introduced  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  is discussed. Stoichiometrically controlled slags were designed from analytical  
374 grade chemicals to serve as precursors for monolithic AAM samples for immobilisation purposes.

375 Under the given experimental conditions, the following conclusions are made:

- 376 a) Very effective immobilisation of  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  was achieved by use of low-alkaline AAMs. An  
377 immobilisation potential of up to 97.6 % and 99.9 % of introduced  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  respectively was  
378 achieved for composition AAM\_1, after 7 days of leaching at 20 °C.
- 379 b) The leaching behaviour of  $\text{Cs}^+$  from the AAMs consists of a combination of initial wash-off,  
380 diffusion and depletion of an easily-leachable fraction.  $\text{Sr}^{2+}$  leaching appears to be limited to a  
381 small fraction present on or near the surface, showing less wash-off and exhibiting slow  
382 depletion.
- 383 c)  $\text{Cs}^+$  immobilisation is dependent on the Si/Al and Ca/(Si+Al) ratios of the precursor while  $\text{Sr}^{2+}$   
384 immobilisation is only dependent on the Ca/(Si+Al) ratio. Better immobilisation is achieved at  
385 lower ratios, independent of the observed differences in precursor fineness or AAM specific  
386 surface area.
- 387 d) Lowering the leaching temperature from 90 °C to 20 °C has a varying effect on the immobilisation  
388 capacity of different compositions. This highlights the importance of being aware that leaching  
389 conditions affect obtained results, especially when comparing compositions. Leaching at higher  
390 temperature affects the curing of the AAMs, which can lead to misinterpretations of leaching  
391 results when comparing immobilisation capacities of different compositions.

392 In general, the developed AAMs show very effective  $\text{Cs}^+$  and  $\text{Sr}^{2+}$  immobilisation which is very  
393 promising for the use of AAMs for waste immobilisation purposes. This study offers a deeper

understanding of the immobilisation mechanism of AAMs, which could encourage further research in finding better alternatives for RAW immobilisation, and, in turn, encourage its large-scale application.

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## Data availability

The raw/processed data required to reproduce these findings cannot be shared at this time as the data also forms part of an ongoing study.

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