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1 Silanization of 3D-printed silica fibers and 2 monoliths

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20 **Abstract**

21 Surface functionalization of complex 3-dimensional porous architectures has not been widely
22 investigated despite their potential in different application domains. In this work, silanization
23 was performed in silica 3D-printed porous structures, and the homogeneity of functional groups

1 within the architecture investigated by comparing the extent of the functionalization in the
2 walls and core of the monolith. A silica ink was used for direct ink writing (DIW) to shape
3 fibers and monoliths with different architectures and stacking designs. The surfaces of the
4 fibers and monoliths were functionalized with 3-aminopropyl(triethoxysilane) (APTES) using
5 different reaction conditions. The nature of the functional groups on the surface, and the
6 presence of $\text{RSiO}_{1.5}$ bonds, were identified by solid state ^{13}C -NMR, ^{29}Si -NMR and by ξ -
7 potential measurements. Elemental analysis was used to quantify the concentration of bonded
8 APTES in the core and walls of the monolith. The availability and hydrolytic stability of the
9 introduced amine group on fibers was evaluated using the adsorption of PdCl_4^{2-} ions within the
10 pH range of 2 to 5. The study found that geometries with interfiber distances above $250\ \mu\text{m}$
11 are homogeneously functionalized with amine groups. As interfiber distance of the monolith
12 decreases, a significantly lower density of amine groups is detected in the core of the monolith.
13 The determination of the homogeneity of 3D-printed monoliths makes this work relevant as it
14 provides the limits of functionalization carried out in stirred batch reactors for geometrically
15 defined structures produced from a 3D-printing process.

16 **Keywords:** silanization, direct ink writing, 3D-printing, silica, APTES, gap-spanning
17 structures, Pd sorption

1 **1. Introduction**

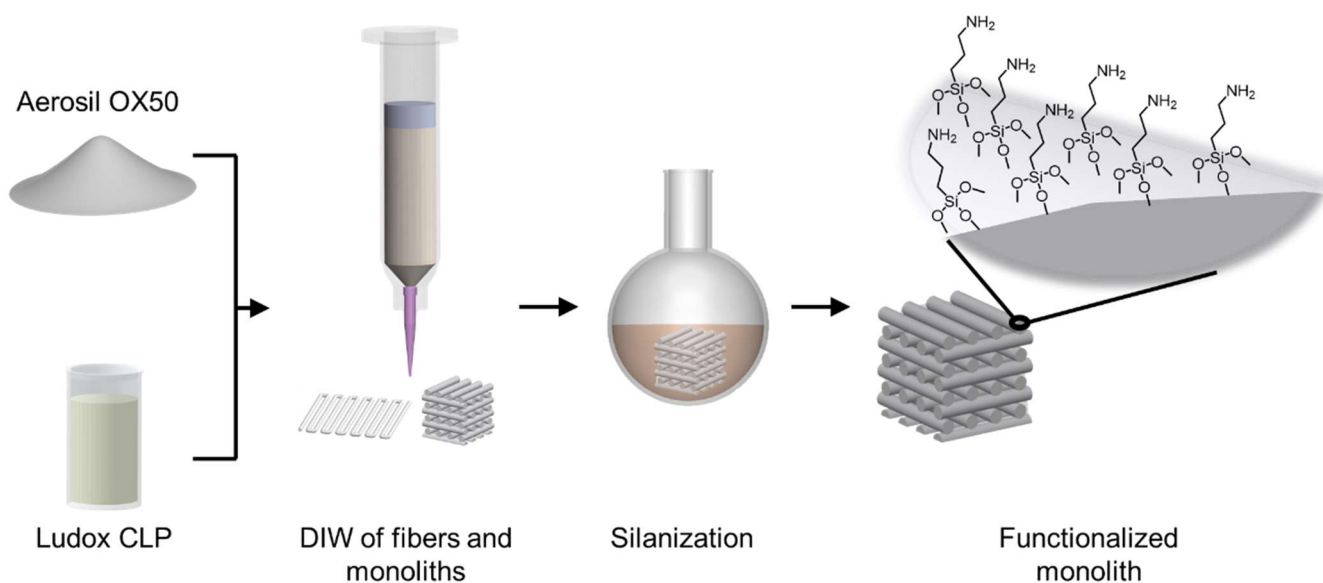
2 Silanization of silica surfaces has been widely described in literature and has been applied
3 in diverse applications such as catalysis, chromatography, and adsorption processes.¹⁻⁷ In
4 particular, adsorption of organic compounds like proteins and polymers, and metals such as
5 palladium (Pd) has been reported for silica functionalized with mercaptopropyl and
6 aminopropyl groups.⁸⁻¹⁰ The reaction between the surface and alkoxy silanes can be performed
7 using diverse protocols including vapor deposition, dipping, perfusion, or in solution with
8 stirred batch reactors.¹¹⁻¹³

9 Silanization of silica powders and spheres have been extensively reported. One of the most
10 common silanization protocols for particles is the functionalization in solution inside stirred
11 batch reactors.¹⁴⁻¹⁶ It is accepted that the silanization occurs homogeneously, understood as a
12 constant density of functional groups throughout the sample, because the silica surface is
13 uniformly exposed to the silanes in solution. Silanization has also been reported for
14 macroscopic silica materials with complex porous architectures such as sol-gel casted
15 structures, capillaries, and more recently 3D-printed monolithic structures manufactured by
16 Direct Ink Writing (DIW).^{11,17-22}

17 The densities of functional groups in silanized macroscopic silica structures have been
18 reported as a constant value by multiple authors.^{17,23,24} Therefore, it has been assumed that the
19 functionalization is homogeneous throughout the structure. Currently, the only report
20 describing silanization of silica gap-spanning structures manufactured by DIW is Thakkar *et*
21 *al* using aminopropyl(triethoxysilane) (APTES), this research reported similar content of
22 nitrogen in functionalized powders than the nitrogen content in the monolith.¹⁷ However, the
23 architecture of the monoliths composed by the fiber diameter, the interfiber distance, and the
24 stacking of each printed layer may have an effect in the extent of functionalization and in the

1 homogeneity of the functional groups density within the monolith. Functionalization
2 homogeneity within the fibers and throughout the monolith could have a direct implication in
3 adsorption processes as higher adsorption capacities could be reached if the surface is fully
4 covered.²⁵ Therefore, to completely understand the potential and limitations of batch
5 functionalization, the geometry and the infill characteristics of the materials manufactured by
6 DIW should be linked with different functionalization conditions. Current state of the art in
7 DIW of silica can be divided between the manufacturing of dense and porous silica structures.
8 Dense structures have been mainly manufactured for optical applications utilizing silica
9 microspheres,²⁶ glass powder,^{27,28} and sol-gel feedstocks.²⁹ On the other hand, studies
10 involving DIW of porous silica structures used powder based,^{17,30,31} and template assisted sol-
11 gel systems.³²

12 The main goal of this work was to assess the homogeneity of the silanization in 3D-printed
13 gap-spanning structures with porous fibers and controlled channeling using a stirred batch
14 reactor. Variations in temperatures, reaction times, and concentrations of silane were used to
15 evaluate the effect of the reaction parameters on the homogeneity of functional groups in the
16 monoliths. To achieve this goal, an ink formulation based on powder and colloidal silica was
17 developed and characterized. Fibers and monoliths were shaped by DIW and characterized by
18 nitrogen sorption, scanning electron microscopy (SEM), and thermogravimetry (TGA). The
19 fibers and monoliths were then silanized with APTES using variations in temperature, reaction
20 time, and concentration in a stirred batch reactor. The occurrence of mass transfer limitations
21 to the interior of the monolith, or within the pore structure of the fibers itself, are investigated
22 using the comparison of the extent of functionalization of ground monoliths. **Scheme 1**
23 illustrates the workflow proposed in this research. This information is used to make practical
24 decisions regarding the functionalization procedures for 3D-printed structures.



1
2 **Scheme 1.** Workflow proposed in this manuscript including mixing, printing, and silanization
3 of the structures with APTES.

4 **2. Experimental**

5 **2.1. Materials**

6 Preparation of the ink was made with Aerosil® OX-50 (OX50) with particle sizes between
7 50 nm and 80 nm supplied by Evonik, LUDOX® CL-P (CLP) with particles of 22 nm donated
8 by Grace, and lanolin purchased from Fagron. The silanization reagent APTES was acquired
9 from sigma, while toluene, triethylamine (TEA), and 4 Å molecular sieves were purchased
10 from VWR. In addition, the toluene was dried with the molecular sieves before the experiment
11 started. Furthermore, the silicone/polyethylene (PE) coated paper was supplied by Aubry
12 Papier. If not stated in the text, all materials and reagents were used as received.

13 **2.2. Silica ink preparation**

14 The ink for DIW was formulated by mixing CLP and OX50 as solids sources, and lanolin
15 as rheology and a drying agent. A standard formulation was prepared by adding 8.9 g of lanolin,

1 50 g of CLP, and 41 g of OX50 in a container suitable for mixing in the planetary mixer
2 SpeedMixer DAC 1400-1000 VAC. The OX50 was added in multiple steps and in every step
3 mixed for two minutes until a total of 41 g were reached.

4 **2.3. 3D-printing of fibers and monoliths**

5 The ink was transferred to a syringe barrel and extruded through conical nozzles.
6 Occasional nozzle blockage, due to the presence of powder agglomerates, was observed with
7 nozzle diameters below 400 μm . Sieving the ink through a mesh of 30 μm using a reusable
8 syringe filter assembly avoided the clogging and resulted in a continuous extrusion. The
9 syringe was installed in a n-Script 3Dn-500 3D-printer, conditioned at 20 °C with a relative
10 humidity between 45% and 55%. All the structures were extruded on top of the PE side of the
11 silicone/PE coated paper. Fibers were extruded continuously using different nozzle diameters
12 of 200 μm , 400 μm , 600 μm , 800 μm , 1100 μm and 1600 μm . Monoliths were printed using
13 either 200 μm or 400 μm nozzles, with two types of stacking designs. Gap-spanning structures
14 were printed as grids to achieve simple cubic structures (SC) and face-centered cubic structures
15 (FCC)³³. Reference images for the SC and FCC internal configurations are shown in **Figure**
16 **S1**.

17 The interfiber distance (IFD) was varied between 150 μm and 250 μm and 1 cm cubes
18 were printed using the configurations described in **Table 1**. The supplemental movie shows the
19 printing of a structure utilizing the formulated ink. After printing, the structures were dried at
20 an average temperature of 20 °C and relative humidity between 45% and 55%. Drying times
21 were approximately 2 hours for the structures with larger gaps, and 48 hours for the finest
22 patterns, No cracking was observed after drying. Next, the structures were removed from the
23 surface of the PE coated paper and placed on top of an alumina plate. The samples were then
24 thermally treated by heating at 60 °C/h to reach 600 °C inside a chamber furnace Nabertherm

1 LH 30/14. The temperature of the furnace was maintained at 600 °C for 4 h before cooling
2 down to room temperature. In addition, thermally treated structures were ground and used as a
3 control sample for the functionalization experiments. The ground monoliths (GM) had a d_{50}
4 particle size of 16 μm (**Figure S2**).

5 **Table 1.** Description of the infill details including interfiber distance (IFD), fiber diameter
6 (FD), and type of stacking used between simple cubic structures (SC), and face-centered cubic
7 structures (FCC).

Sample ID	Nozzle diameter (μm)	IFD set (μm)	Stacking	FD after thermal treatment (μm)	IFD after thermal treatment (μm)
200/250-SC	200	250	SC	206 \pm 18	241 \pm 14
400/250-SC	400	250	SC	354 \pm 20	253 \pm 15
200/150-SC	200	150	SC	213 \pm 18	141 \pm 15
200/150-FCC	200	150	FCC	194 \pm 12	153 \pm 19

8

9 **2.4. Silanization of 3D-printed fibers and ground monoliths**

10 Silanization with aminopropyl-alkoxysilanes has been researched because its use in diverse
11 applications,^{7,14,34,35} the particularity of the chain bending towards the surface,^{11,36,37} and as it
12 is a self-catalytic reaction that can be performed in gas phase or in liquid phase.^{15,38} In this
13 work, silanization of 3D-printed fibers and GM was performed in solution in a batch stirred
14 reactor. All samples and glassware were stored at 75 °C prior to silanization. The solids were
15 functionalized by silanization based on a protocol described in the literature.³⁶ APTES and

1 TEA were added into a container, mixed under a nitrogen stream and a 60 mL syringe filled
2 with the resulting reaction mixture. Simultaneously, known masses of 3D-printed silica fibers
3 and GM were placed separately in a two neck round bottom flask. A vacuum line with a valve
4 was attached to one of the necks and the flask sealed by a rubber septum on the other neck.
5 Vacuum was induced into the flask for 3 to 5 minutes before closing the valve. The rubber
6 septum in the two-neck flask was penetrated with the syringe containing the reaction mixture
7 that was sucked into the flask by the vacuum and resulted in the immediate impregnation of
8 the material. The vacuum line was removed from the flask to be replaced by a condenser.
9 Afterwards, the solution with the solids was stirred at 50 rpm for 2 h or for 24 h. The samples
10 were filtered using 0.25 μm cellulose fiber filters, flushed with nitrogen, and washed three
11 times sequentially with acetone, water, and acetone. After washing the samples were flushed
12 with a nitrogen stream, dried at 75 °C for 24 h, and stored in closed vials in an oven at 75 °C
13 to limit water adsorption by the surface.

14 **2.5. Silanization kinetics of 3D-printed monoliths**

15 The kinetics of the silanization reaction were investigated on silica monoliths with the
16 configuration 200/150-SC. The monoliths were vacuum impregnated using a 20 mM solution
17 of APTES in toluene and TEA (3:1 ratio for each mol of APTES) and reacted over time under
18 reflux conditions. The structures were reacted using time intervals ranging from 0.5 h to 24 h
19 in a round bottom flask that performed the function of a batch reactor. The samples were
20 washed with acetone, followed by a washing/hydrolysis step using water and washed again
21 using acetone. All washing steps were done using vacuum impregnation processes. The
22 washing was followed by drying the structures in an oven at 60 °C for 24 h.

23

24

1 2.6. Extent of silanization and homogeneity in 3D-printed structures

2 Two silanization protocols were applied to assess the extent and the homogeneity of the
3 functionalization between the wall and the core of the monoliths. All samples and glassware
4 were stored at 75 °C prior to being used in the silanization. In the first procedure, the reactions
5 were maintained at room temperature, under reflux with dry toluene as solvent, APTES as
6 reagent, and TEA as the reaction promotor. The stoichiometry was based on a theoretical
7 hydroxyl density of 2.1 #OH/nm².³⁹ The experiment involved adding toluene, APTES, and
8 TEA (a 1:3 ratio of APTES:TEA) into a round bottom flask. Silanol:APTES ratios equal to
9 1.1:1 or 1:7, depending on the treatment, were used in the mixtures. The solution was mixed
10 under a nitrogen stream and the reaction mixture placed inside a 60 mL syringe. Next, a known
11 mass of 3D-printed monolith was placed into a two neck round bottom flask. A vacuum line
12 with a valve was attached to one of the necks and the flask sealed by a rubber septum on the
13 other neck. A vacuum (minimum pressure = 100 mbar) was induced into the flask for 3 to 5
14 minutes before the valve was closed. The rubber septum in the two-neck flask was penetrated
15 with the syringe containing the reaction mixture that was then sucked into the flask, resulting
16 in the immediate impregnation of the monolith. The vacuum line was removed from the flask
17 to be replaced by a condenser. The functionalization conditions are listed in **Table 2**. The
18 samples were taken out of the solution, flushed with nitrogen, washed three times sequentially
19 with acetone, water, and acetone. The samples were dried by flushing with a nitrogen stream,
20 and further treated at 75 °C for 24 h. The cores and the walls of the monoliths were cut as
21 pictured in **Figure S3** using a diamond blade of 500 µm rotating at 2000 rpm without water,
22 while moving the sample at a speed of 0.02 mm/s.

23 A second procedure adapted from Krasnoslobodtsev and Smirnov was developed to
24 increase the extent of functionalization at the surface of the monoliths, and to reduce the

1 reaction time.³⁸ This procedure was performed using multiple vacuum wetting by forcing fresh
 2 APTES into the unreacted pores. In this procedure, monoliths of 400/250-SC cubic-like shape
 3 and a silanol:APTES ratio equal to 1.1:1 (APTES 2.5 mM concentration) were maintained at
 4 room temperature for 0.5 h. The samples were washed after synthesis using vacuum
 5 impregnation washing processes first with acetone, followed by a washing/hydrolysis step
 6 using water, and a second washing with acetone. The samples were then dried in an oven at 80
 7 °C for 30 min and the reaction and washing steps repeated two more times. This treatment was
 8 labeled as 2.5-0.5-RT-X3. All the reaction experiments were performed in duplicate.

9 **Table 2.** Experimental conditions for APTES functionalization of silica monoliths.

Silanization code	Concentration (mM)	Time (h)	Temperature (°C)
20-0.5-RT	20	0.5	20
20-0.5-Ref	20	0.5	110
20-24-RT	20	24	20
20-24-Ref	20	24	110
2.5-0.5-RT	2.5	0.5	20
2.5-0.5-Ref	2.5	0.5	110
2.5-24-RT	2.5	24	20
2.5-24-Ref	2.5	24	110

10

11

1 2.7. Pd adsorption experiments

2 The availability of the amine groups to interact with the environment was verified by
3 performing Pd adsorption experiments, using untreated fibers and fibers functionalized with
4 APTES. The influence of pH in the adsorption of Pd was studied at pH 2.0 ± 0.1 , 3.0 ± 0.1 , 4.0
5 ± 0.1 , and 5.0 ± 0.1 . Since the Pd speciation strongly depends on the pH of the solution and the
6 chloride concentration, a solution of Pd with a concentration of 150 mg/L at pH 1 was prepared
7 by dissolving palladium dichloride (PdCl_2 , Sigma Aldrich) in hydrochloric acid (HCl) for 24 h
8 to ensure a fixed concentration of chlorine (Cl). Stock solutions of Pd adjusted to pH 2, 3, 4,
9 and 5 were prepared with sodium hydroxide (NaOH) solutions to determine the maximum
10 adsorption capacity for Pd adsorption. For each adsorption experiment, 200 mg of fibers were
11 placed in a sample holder with a bottom polyethylene mesh (350 μm , PVF GmbH) to avoid
12 mechanical damage to the fibers. The sample holder was inserted into a plastic vial, 20 ml of
13 the Pd solution was added, and the system was stirred at 300 rpm for 24 hours with a magnetic
14 stirrer located between the plastic vial and the sample holder. All experiments were performed
15 in duplicate. The Pd and silicium (Si) concentrations in the starting solutions, as well as in the
16 solutions after adsorption, were measured by inductively coupled plasma optical emission
17 spectroscopy (ICP-OES, Agilent Technologies 5100). The adsorption capacity (Q_e) is
18 calculated from **Equation 1** where m_e is the mass of adsorbant (g), C_o is the initial
19 concentration of the metal in the solution in mg/L, C_e is the concentration of the metal in
20 equilibrium in mg/L, and V is the volume of solution in L.

21 Equation 1

$$22 \quad Q_e = \frac{C_o - C_e}{m_e} V$$

23

1 2.8. Characterization

2 Rheological characterization of the ink was made in a Thermo Haake MARS 60 instrument
3 with 3.5 cm diameter parallel plates for oscillatory experiments, and with 3.5 cm and 2° angle
4 cone and plate for the steady state experiments. For oscillatory experiments, the measurements
5 were made by conditioning the ink for 10 minutes at a shear stress of 0.001 Pa using 2% strain,
6 followed by a shear stress swap between 0.001 Pa and 1000 Pa with 2% strain. Steady state
7 experiments were performed by conditioning the sample for 5 minutes with a shear rate of 0.01
8 s⁻¹. The shear rate was varied between 0.001 s⁻¹ and 100 s⁻¹.

9 Solid contents of the inks were obtained by placing a known mass of the ink on a heating
10 plate and heating at 60 °C/h to reach 600 °C in a Nabertherm LH 30/14 chamber furnace. The
11 temperature was then maintained for 4 h before cooling down to room temperature. The weight
12 was measured, and a second thermal treatment was done to verify the final weight.
13 Determination of the interconnectivity of the pores was performed by Hg intrusion porosimetry
14 using a PASCAL 140/240 porosimeter. Pore diameter and pore volume were calculated by
15 BJH from nitrogen sorption isotherms, after degassing the samples at 100 °C and 0.01 mbar,
16 measured in an autosorb iQ2 MP instrument (Quantachrome GmbH). Furthermore, the specific
17 surface area (SSA) was calculated by the Brunauer–Emmett–Teller (BET) model. Hydroxyl
18 quantification was performed based on the work of Mueller *et al*³⁹ that used the SSA and the
19 weight loss calculated from TGA using a NETZSCH STA 449C instrument. For TGA, the
20 sample was heated in a nitrogen atmosphere (70 mL/min) from 25 °C to 120 °C at 10 °C/min,
21 then held at 120 °C for 10 min, and followed by a heating ramp from 120 °C to 800 °C at 20
22 °C/min. In the final step, the sample was maintained at a temperature of 800 °C for 10 min.

23 The structure homogeneity and the infill patterns of the printed structures were examined
24 by optical microscopy. In order to do so, the fiber diameter (FD) and the IFD were measured

1 in different sections of each monolith. Reported values were collected from the cross section
2 of the monolith and are based on more than 50 measurements in the top, middle, and bottom
3 positions. The images were acquired using a Zeiss Discovery V12 stereomicroscope, equipped
4 with a Plan Apo S 1.0x FWD 60 mm objective and image collection performed using an
5 Axiovision MRc digital camera connected to the microscope. SEM-EDS images were acquired
6 using a Nova Nano SEM 450 (FEI, USA) cold field emission scanning electron microscope
7 (FEGSEM) operating at an acceleration voltage of 5 kV. Quantification of carbon and nitrogen
8 in the samples was made by elemental analysis using a Elementar vario EL cube. ξ -potential
9 measurements were performed for cores and walls of the sample 200/150-SC and 400/250-SC,
10 using the treatment 20-24-Ref, as well as a control sample without functionalization in the
11 surface that serves as a reference. The ξ -potentials were identified on a ZetaSizer Nano ZS
12 instrument (Malvern Panalytical) by grinding the monoliths and suspending 20 mg of the
13 ground powder in 10 mL of a 10 mM potassium chloride (KCl) solution. The suspension was
14 divided into aliquots and the pH of each aliquot adjusted to more basic or acid pH using 0.01
15 M, 0.1 M and 1 M solutions of NaOH or HCl and the isoelectric points (IEP) were calculated
16 by interpolation.

17 Formation of bonds between the silica surface of the monoliths and the APTES molecules
18 was followed by solid state NMR using the walls of the samples after cutting as seen in **Figure**
19 **S3**. Solid-state ^{13}C -CPMAS (Cross-Polarization Magic Angle Spinning) NMR spectra were
20 acquired on a Bruker 400 MHz spectrometer (9.4 Tesla) equipped with a 4 mm probe and
21 magic angle spinning performed at 7 kHz using ceramic zirconia rotors. Furthermore, the
22 aromatic signal of hexamethylbenzene was used to calibrate the carbon chemical shift scale
23 (132.1 ppm). The acquisition parameters used were: a spectral width of 50 kHz, a 90° pulse
24 length of 3.5 μs , an acquisition time of 20 ms, a recycle delay time of 3 s, a spin-lock field of

1 50 kHz, a contact time of 1 ms, and 75000 accumulations. During acquisition, the high-power
2 proton dipolar decoupling was set to 70 kHz.

3 Solid-state ^{29}Si -CPMAS NMR spectra were acquired on an Agilent VNMRS DirectDrive
4 400 MHz spectrometer (9.4 Tesla) equipped with a T3HX 3.2 mm probe and magic angle
5 spinning performed at 6.5 kHz using ceramic zirconia rotors. The talc signal was used to
6 calibrate the silicon chemical shift scale (-98 ppm). Acquisition parameters used were: a
7 spectral width of 24 kHz, a 90° pulse length of 3.2 μs , an acquisition time of 15 ms, a recycle
8 delay time of 5 s, a spin-lock field of 80 kHz, a contact time of 2 ms, and 75000 accumulations.
9 High power proton dipolar decoupling during the acquisition time was set to 80 kHz.

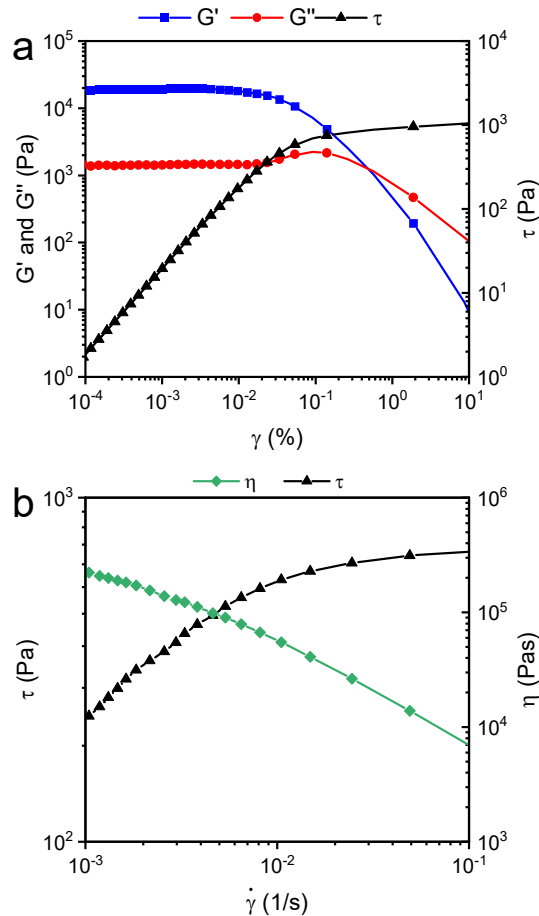
10 Solid-state ^1H -MAS homonuclear dipolar decoupled NMR spectra were acquired on a Jeol
11 ECZ600R 600 MHz spectrometer (14.1 Tesla wide bore magnet) equipped with a 3.2 mm wide
12 VT Range HXMAS probe. Magic angle spinning was performed at 19.5 kHz and proton-proton
13 homonuclear dipolar decoupling performed using a wPMLG-5 pulse sequence. Glycine was
14 used to calibrate the proton chemical shift scale and the peaks set at 3.4 ppm and 4.4 ppm (CH_2
15 protons), and 8.5 ppm (NH_2). The acquisition parameters used were a spectral width of 55 kHz,
16 a 90° pulse length of 2.3 μs , an acquisition time of 20 ms, a recycle delay time of 20 s, and 32
17 accumulations.

18 **3. Results and discussion**

19 **3.1. Characterization of silica ink for direct ink writing**

20 The printability of the silica ink to manufacture monoliths with different configurations
21 was correlated from viscoelastic and flow experiments after preparation of the ink. A major
22 attribute of the mixed ink is the formulation using silicas with two defined particle sizes that
23 enable printing below the pressure limit of the printer (100 psi) while maintaining a solid

1 content of 64 %.⁴⁰ The viscoelastic behavior of the ink is displayed in **Figure 1a**. The elastic
 2 modulus (G') of the ink is 10000 Pa higher than the viscous modulus (G'') within the linear
 3 viscoelastic region, indicative of a solid-like behavior when low shear stress is applied. Also,
 4 in **Figure 1a** the crossing between G' and G'' occurs at a shear stress (τ_f) value of 900 Pa. As
 5 a result, once the ink is extruded, the formed fibers retain their shape, even when stacked into
 6 several layers. Furthermore, based on the rheology data shown in **Figure S4** intensive mixing
 7 was required to achieve homogeneous inks. The ratio between the value of G' in the linear
 8 viscoelastic region and τ_f , known as the Feilden's figure of merit (Φ), was 22.5 which is higher
 9 than the printability limit of 20.^{41,42} In addition, the steady state graph in **Figure 1b** shows an
 10 increase of the shear stress as the shear rate increases. This behavior is typical of non-
 11 Newtonian fluids and is beneficial for printability as the viscosity is reduced in function of the
 12 shear stress, further demonstrating that this ink is suitable for DIW.



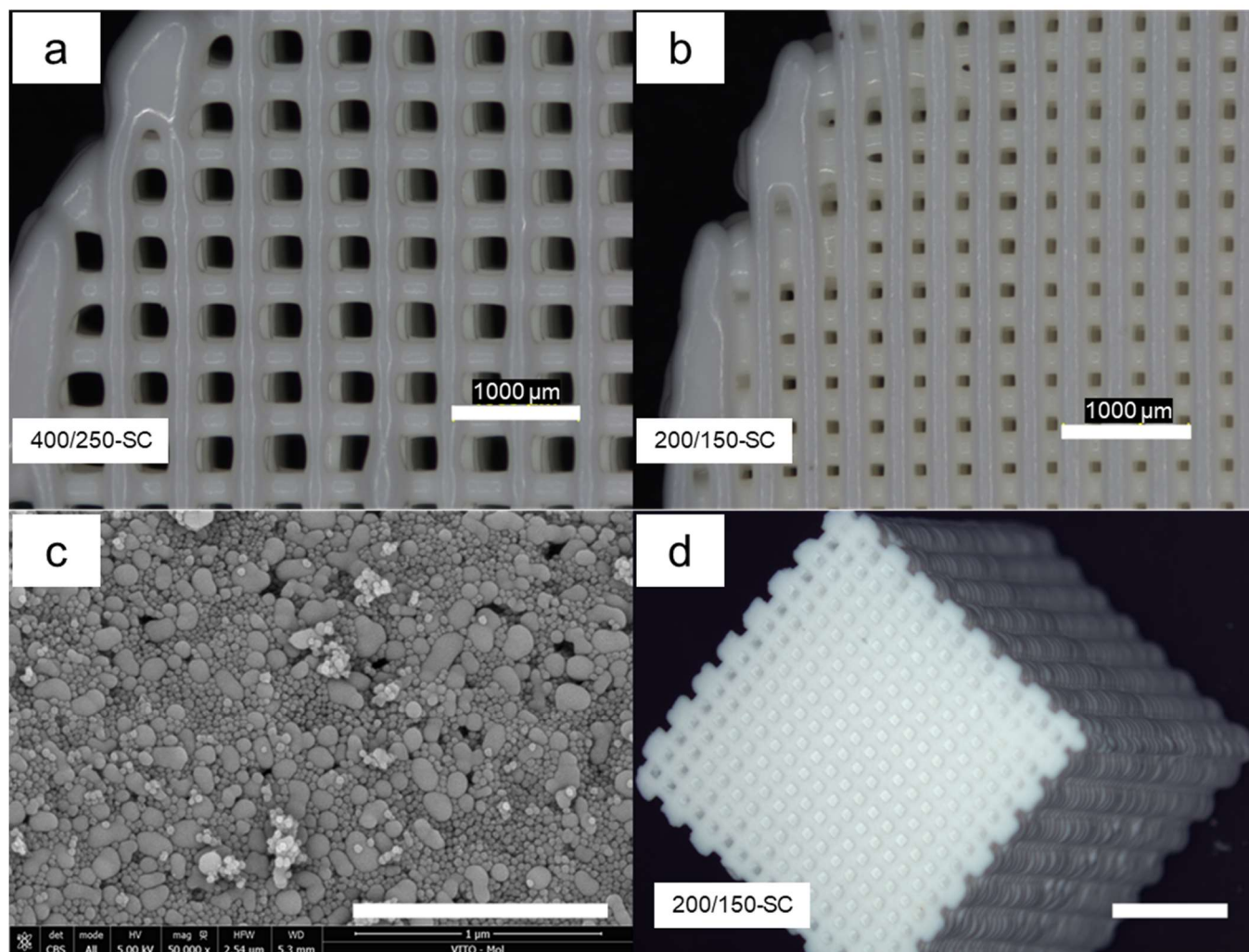
1 **Figure 1.** Evolution of the elastic modulus (G'), the viscous modulus (G'') and the shear stress
2 (τ) in function of the imposed strain (γ) to evaluate the viscoelastic behavior of the ink (a), and
3 evolution of the dynamic viscosity (η) and τ in function of the shear rate, showing the shear
4 thinning behavior of the ink (b).

5 **3.2. Printing and printed structures**

6 The printable ink was used to print fibers and monoliths that could be further
7 functionalized. The diameters of these fibers after thermal treatment were $172 \pm 3 \mu\text{m}$, $356 \pm$
8 $3 \mu\text{m}$, $505 \pm 1 \mu\text{m}$, $747 \pm 4 \mu\text{m}$, $1028 \pm 3 \mu\text{m}$, and $1403 \pm 3 \mu\text{m}$. Optical microscopy images of
9 the fibers are shown in **Figure S5**. **Figure 2a** and **Figure 2b** show the images from optical
10 microscopy of the top surface of the monolith, demonstrating that printing of monoliths is
11 possible for IFD higher than $150 \mu\text{m}$ for the $200 \mu\text{m}$ nozzle, and higher than $250 \mu\text{m}$ for the
12 $400 \mu\text{m}$ nozzle. Further decreasing the IFD resulted in merging of the fiber extrudate with the
13 adjacent fibers thereby closing the openings of the monolith (**Figure S1**). FD and IFD are
14 almost identical along the structure as seen in **Figure S6** and **Figure S7**. The average FD and
15 IFD measured from OM images is reported in **Table 1**. Therefore, the monoliths are regarded
16 as homogeneous and they have reproducible porous architectures.

17 Microstructural analysis of the surface of the silica monoliths reveals a bimodal
18 distribution of sphere-like particles as observed by SEM and shown in **Figure 2c** and **Figure**
19 **S8**. Smaller spheres of about 22 nm correspond to the size reported by the manufacturer for
20 colloidal silica, while larger spheres between 50 nm and 80 nm match with the reported value
21 for the fumed silica used in this work. It is important to note that no agglomerates of fumed
22 silica were seen, which is indicative of the correct mixing and homogeneity of the ink. The
23 pore size distribution measured by Hg intrusion (**Figure S10**) and calculated by BJH from

1 nitrogen sorption measurements (**Figure S9**) demonstrate that the structures are mainly
2 mesoporous.



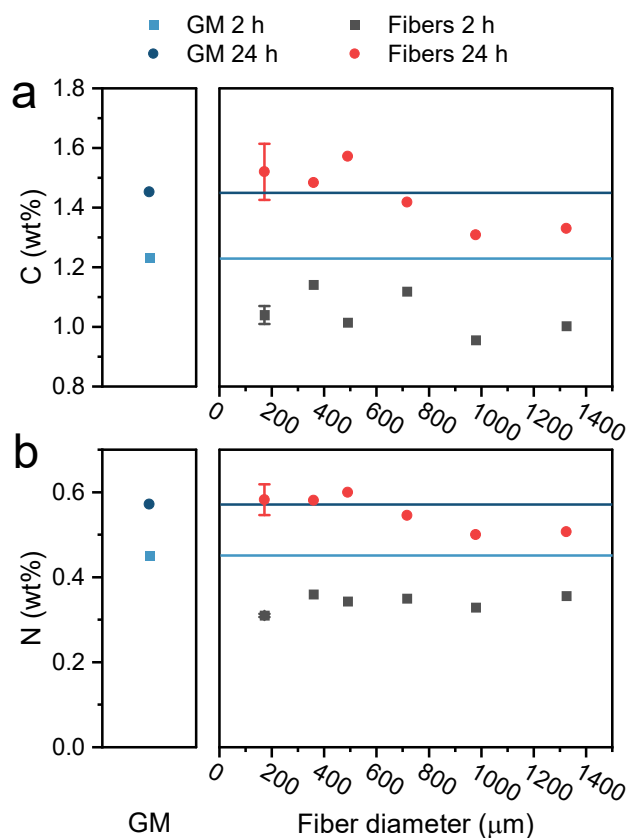
3
4 **Figure 2.** Optical microscopy of the top surface of a 400/250-SC monolith (**a**) and a 200/150-
5 SC monolith (**b**); SEM image of the monolith surface showing a bimodal distribution between
6 colloidal and fumed silica (**c**); cubic structure used in the functionalization experiments (**d**).
7 Scalebars represent 1 μm, for **c**; and 3 mm for **d**.

8 **3.3. Functionalization of silica ground monoliths and fibers**

9 Ensuring a full access of APTES within the interior of each extruded fiber is required to
10 reach full functionalization. The approach followed in this work consisted in the silanization

1 of GM and extruded silica fibers (ESF) and comparing the extent of their functionalization
2 thereby avoiding the complexities of 3D-printed geometries. GM and ESF were functionalized
3 with APTES using the first reaction procedure. **Figure 3** compares the evolution of the carbon
4 and nitrogen content for different fiber diameters after reaction times of 2 h and 24 h. After 24
5 h of reaction 1.45 wt% of carbon and 0.57 wt% of nitrogen were measured in the functionalized
6 GM using elemental analysis. The percentages obtained were recalculated as 1.21 mmol/g for
7 carbon and 0.41 mmol/g for nitrogen. These results are regarded as the maximum values of the
8 degree of functionalization under these reaction conditions, and the silica used in this work.
9 They serve as benchmark values for the evaluation of the functionalization extent of extruded
10 fibers and monoliths. From reports on hydroxyl density, the hydroxyl content in silica thermal
11 treated at 600 °C before functionalization is in the range of 1.0 to 2.5 #OH/nm² or 0.12 to 0.29
12 mmol OH/g.^{39,43} Therefore, it can be concluded from the elemental analysis results that 1.4 to
13 3.4 amine groups are bonded for each hydroxyl on the surface.

14 Fibers, regardless of the diameter, show a decrease of ~15% in carbon and nitrogen content
15 after 2 hours of reaction compared to the values of the GM sample (**Figure 3**). After 24 hours
16 the fibers with diameters below 800 μm show similar carbon and nitrogen contents compared
17 to those of GM. On the other hand, fibers with diameters larger than 800 μm still show ~10 %
18 lower carbon and nitrogen content compared to those of GM. This is indicative of mass
19 diffusion limitations occurring in the pore system of the fibers, leading to slower reaction
20 kinetics. This can be explained by the narrow pore system of the fibers due to the dense particle
21 packing inside the fibers and the absence of macropores, as measured by nitrogen sorption and
22 mercury intrusion (**Figure S9** and **Figure S11**). One approach to overcome these diffusion
23 limitations could be to further prolong the reaction time to reach less accessible pores.
24 Consequently, to avoid diffusion limitations observed in the silanization of fibers, the 3D-
25 printed structures were printed using 200 μm and 400 μm nozzles.



1

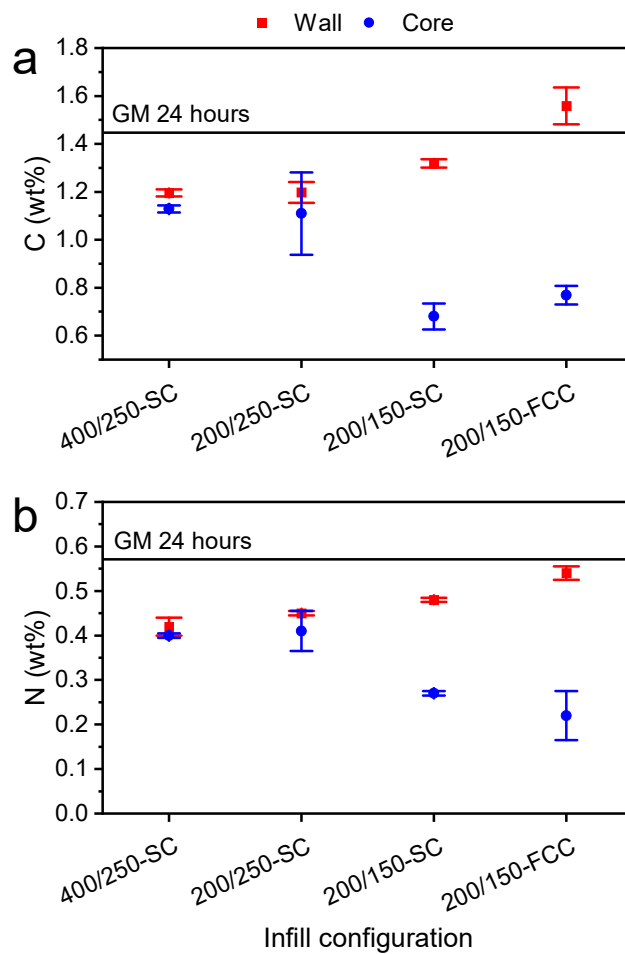
2 **Figure 3.** Concentration of carbon (a.) and nitrogen (b.), obtained by elemental analysis after
 3 silanization of GM and fibers of different diameters with 10 mM APTES solution in toluene
 4 and 3x excess triethylamine under reflux for 2 h and 24 h.

5 3.4. Functionalization of silica 3D-printed monoliths

6 Additionally to the diffusion within a fiber, homogeneous functionalization could be dependent
 7 of the internal configuration of the structure. Monoliths manufactured with different stackings,
 8 fiber diameters, and interfiber distances were reacted under controlled conditions using a batch
 9 reactor. These experiments were performed to explore if the configuration of the channels in
 10 the monolith could have a direct impact on the homogeneity of functional groups within the
 11 monolith. Different reaction conditions were evaluated to understand if possible diffusion
 12 limitations could be avoided by the silanization protocol.

13 3.4.1. Effect of the geometry

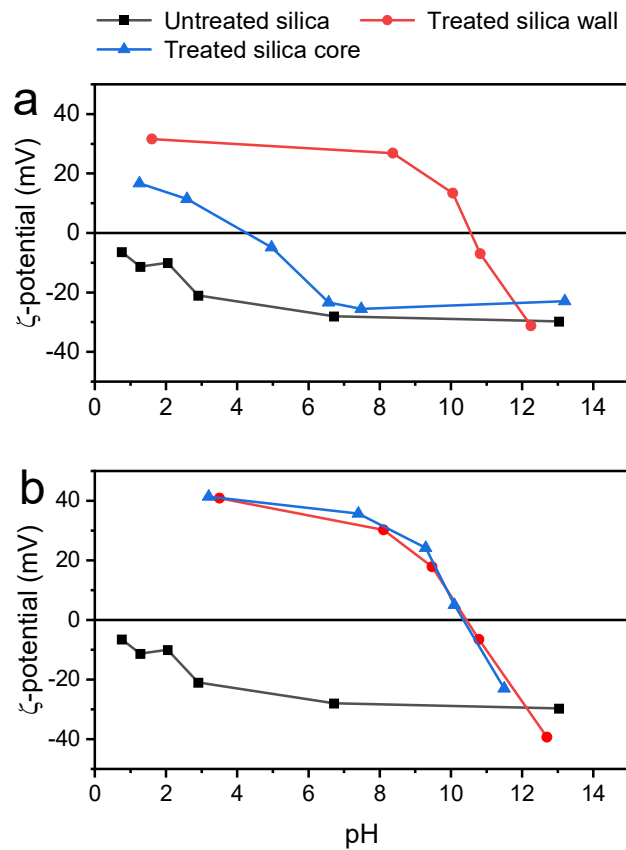
1 Carbon and nitrogen content of the functionalized samples 400/250-SC and 200/250-SC
2 are lower than that of the functionalized GM as **Figure 4** shows, and no significant differences
3 between the core and wall are observed. As the interfiber distance of the monolith decreases
4 (200/150-SC and 200/150-FCC), differences in elemental composition between walls and core
5 are observed, with twice as much carbon in the walls than in the cores. Therefore, the interfiber
6 distance that drives the macro channeling inside the sample is a limiting factor in achieving a
7 homogeneous functionalization using this protocol. Furthermore, the stacking design (SC or
8 FCC) is not a determining factor for the homogeneity of functionalization. The results in
9 **Figure 4** are conclusive on a threshold value of the IFD to obtain a homogenous coverage and
10 intrusion of APTES using the silanization conditions. From these data, the threshold is between
11 150 μm and 250 μm .



1 **Figure 4.** Percentage of carbon (**a**) and nitrogen (**b**) after silanization with APTES in toluene
2 under reflux for 24 h as determined by elemental analysis of the monoliths 400/250-SC,
3 200/250-SC, 200/150-SC, and 200/150-FCC. The horizontal solid line represents the
4 maximum functionalization reached in GM after 24 hours.

5 **3.4.2. ζ -potential**

6 The IEP and the shape of the ζ -potential curves are indicators for the extent of
7 functionalization and homogeneity of the functional groups on the surface. From **Figure 5** it
8 can be seen that the control sample did not reach a ζ -potential equal to zero. This is in agreement
9 with previous evidence where silica suspensions below pH 3 become unstable due to
10 dissolution and reorganization of the silica.⁴⁴ The functionalized core of sample 200/150-SC
11 has an interpolated IEP of 4.3, while the highly functionalized wall has an interpolated IEP of
12 10.6. Typically, the IEP of silica treated with APTES is between 7.6 and 8.4.^{34,45,46} It is possible
13 that the presence of alumina on the surface of CLP contributes to a larger IEP.⁴⁷ The shape of
14 the curve in **Figure 5** gives additional information about the chemical configuration of the
15 surface.^{48,49} A sharp transition between positive and negative ζ -potential values represents a
16 highly homogeneous surface as seen for the walls of 200/150-SC and 400/250-SC, and the core
17 of 400/250-SC. In addition, a gradual transition between positive and negative ζ -potential
18 values typically represents a surface with different functionalities. This is the case of the core
19 in sample 200/150-SC where the surface is composed of amine and hydroxyl groups due to the
20 much lower degree of functionalization (**Figure 4**). Therefore, the results validate that the
21 homogeneity of the functionalization is dependent of the interfiber distance in gap-spanning
22 structures.



1

2 **Figure 5.** ζ -potential measurements at different pH values for determination of isoelectric
 3 points in 200/150-SC monolith (a), and 400/250-SC monolith (b). The lines are traced as
 4 reference and do not represent a model. The horizontal line in ζ -potential = 0 mV can be use
 5 as reference to visualize the isoelectric point in the graph.

6 3.4.3. Effect of the silanization conditions

7 Concentration, temperature, and time of reaction play a dominant role in the silanization.³⁶

8 A complete understanding of these parameters could lead to insights needed to obtain
 9 homogeneous coverage of the surface by the end of the synthetic procedure. Based on the
 10 results displayed in **Figure 6** the extent of the functionalization, as determined from the
 11 elemental composition, is dependent of the conditions of the silanization. The concentration of
 12 carbon and nitrogen for the walls of 400/250-SC and 200/150-SC structures is similar in each
 13 silanization treatment.

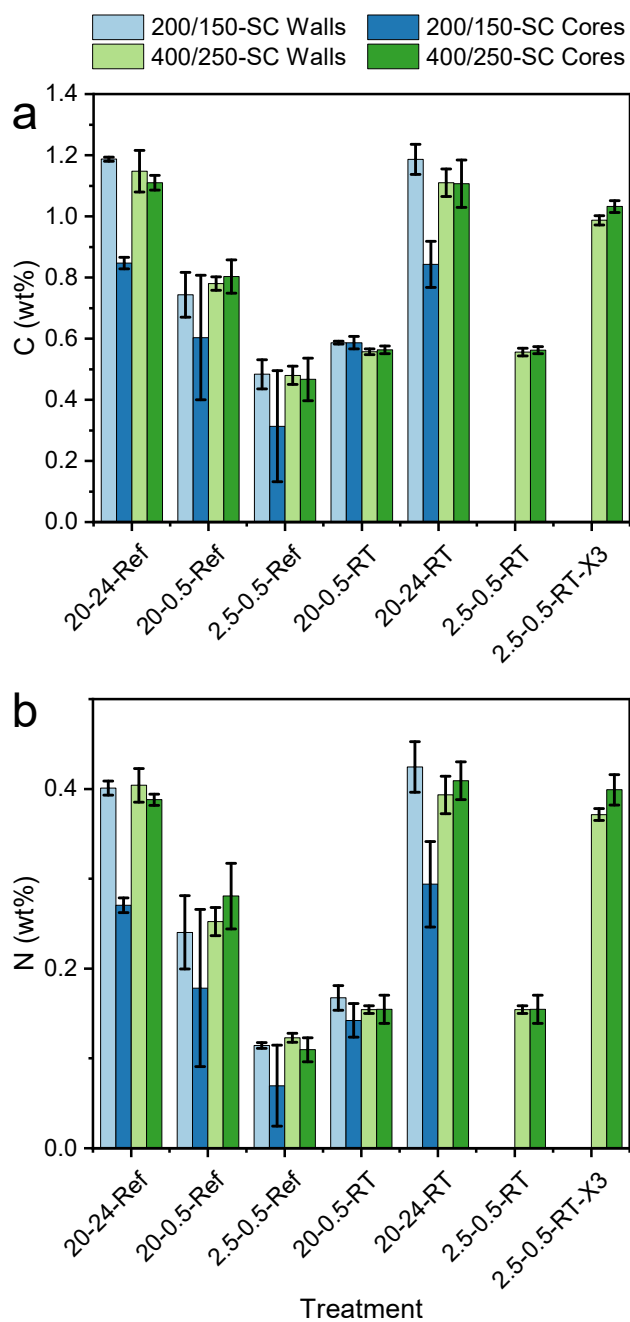
1 The concentration of APTES does have an effect in the extent of functionalization. From
2 **Figure 6** the amount of carbon and nitrogen on the monoliths after the treatment 20-0.5-Ref,
3 which has a theoretical excess of APTES related to the hydroxyls in the surface, is 30 % higher
4 than the amount of carbon and nitrogen on the monoliths after the treatment 2.5-0.5-Ref, which
5 has not enough APTES to fully functionalize the surface. Notably, the excess of APTES only
6 has a small impact in the coverage of the surface. Therefore, it is recommended to use a slight
7 excess of APTES for vacuum impregnation and further reaction. The extent of
8 functionalization was similar for the samples 200/150-SC and 400/250-SC and no significant
9 differences were observed between the extent of functionalization of the core and the walls in
10 each sample. Therefore, under this conditions there is no effect of the concentration over the
11 homogeneity of the reagent in the sample.

12 Different reaction temperatures do not have an effect for reactions performed for 0.5 h
13 when APTES is used as limiting reagent as seen for the treatments 2.5-0.5-Ref and 2.5-0.5-RT
14 in **Figure 6**, where the extent of functionalization is the same in the two treatments and no
15 significant differences are identified in the percentage of carbon or nitrogen on the cores and
16 on the walls. However, if an excess of APTES is used, the reflux of toluene in the treatment
17 20-0.5-Ref enhanced the surface coverage by 25% related with the reaction at room
18 temperature using the treatment 20-0.5-RT. Therefore, refluxing is recommended for
19 treatments performed for 0.5 h. On the other hand, when the reactions lasted 24 h, the extent
20 of silanization was similar at different temperatures as observed for treatments 20-24-RT and
21 20-24-Ref in **Figure 6**. The treatments 20-24-RT and 20-24-Ref led to homogenous
22 functionalization on the sample 400/250-SC. Contrary, the sample 200/150-SC has different
23 content of carbon and nitrogen between the core and the walls showing the lack of homogeneity
24 previously described in samples with interfiber distances of 150 μm .

1 The most critical silanization parameter to reach homogeneity between the core and the
2 walls for 200/150-SC monoliths is therefore the reaction time. Treatment 20-24-Ref and 20-
3 24-RT are directly related to non-homogeneity of amine groups in the monolith surface.
4 However, the samples reacted with the treatments 2.5-0.5-Ref, 20-0.5-Ref, and 20-0.5-RT
5 have similar contents of carbon and nitrogen on the cores and the walls. This similarity shows
6 that for short reaction times, the reaction proceeds homogeneously throughout the sample,
7 independent of the fiber diameter and interfiber distance. Furthermore, the homogeneity after
8 0.5 h is most likely attributed to an excellent wetting of the surface with the APTES solution
9 achieved through vacuum impregnation. These results are comparable to the functionalization
10 of GM and fibers with different diameters after 2 h of reaction time (**Figure 3**).

11 The reaction kinetics with 20 mM APTES solutions were carried out at room temperature
12 and under reflux (**Figure S13**) considering that samples 200/150-SC were homogeneous after
13 0.5 h and non-homogeneous after 24 h. Consequently, it can be concluded from the kinetics
14 plots that the extent of functionalization progress homogeneous through the sample the first
15 0.5 h, independent of the configuration, and over time, the diffusion of the reagent through the
16 monolith channels plays a significant role in the final concentration of carbon and nitrogen in
17 the walls and the core of the monolith. It is noteworthy that the maximum amount of carbon
18 obtained in the walls of 200/150-SC, and in the core and walls of 400/250-SC, after treatment
19 with 20-24-Ref and 20-24-RT is similar to that of the ESF and the GM experiments. Therefore,
20 it can be concluded that the inhomogeneity in the samples after 24 hours is induced by diffusion
21 limitations and lack of flow through interfiber channels of 150 μm . As a result, the APTES
22 molecules are prevented from reaching the cores of the monoliths. These results, combined
23 with the evaluation between geometries, infer that the interfiber distance for homogeneous
24 functionalization is located between 150 μm and 250 μm .

1



2

3 **Figure 6.** Elemental analysis results of functionalized silica monoliths under different APTES
4 functionalization treatments. Weight percentage of carbon (a), and weight percentage of
5 nitrogen (b).

6

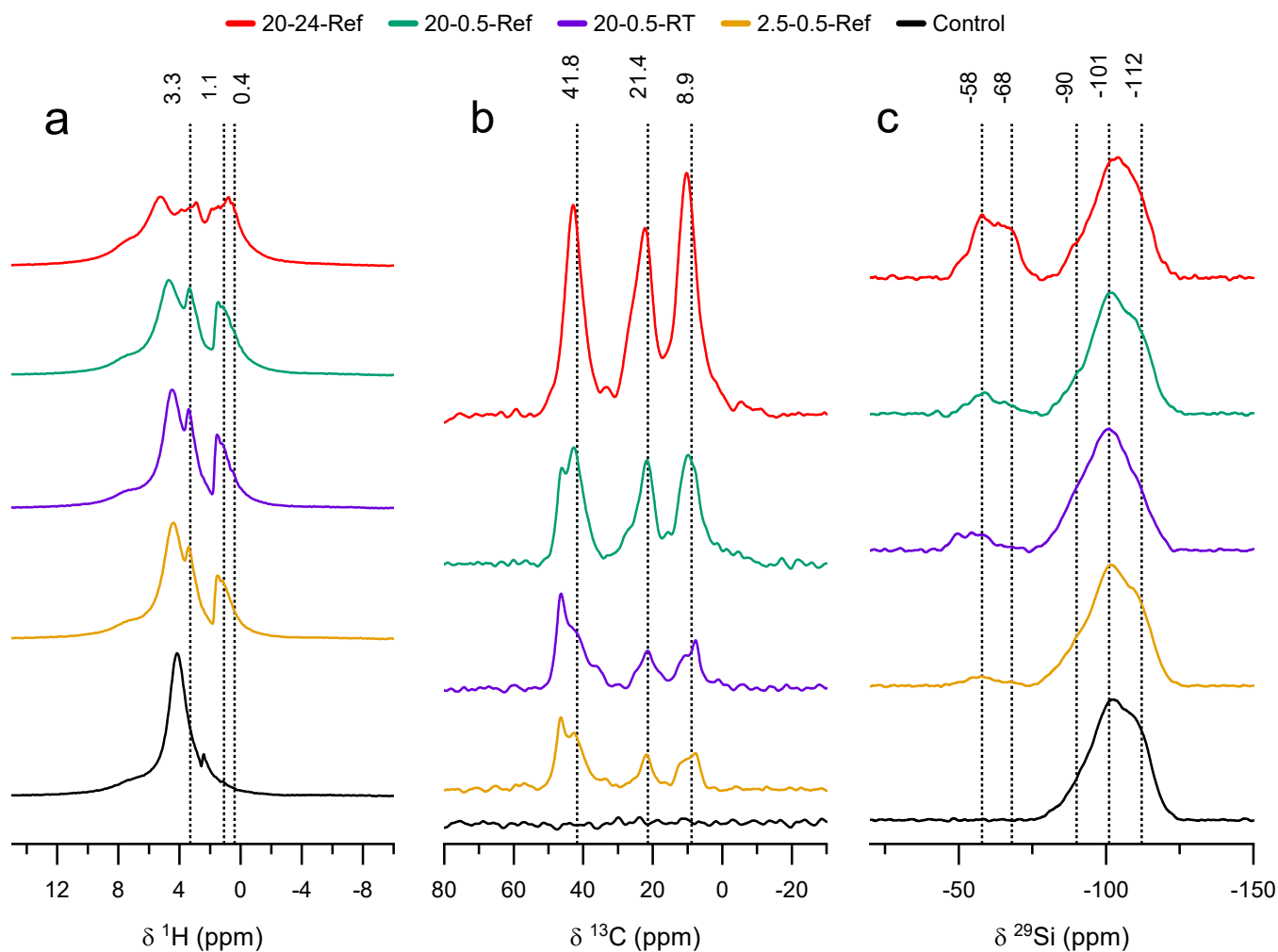
3.4.4. Bonding of APTES to silica surfaces analyzed by ^1H -MAS, ^{13}C -CPMAS, and ^{29}Si -CPMAS NMR

The ^1H -MAS NMR spectrum of the control sample, shown in **Figure 7a**, has a single peak at $\delta = 4.8$ ppm, this is assigned to silanol groups on the surface interacting with water as illustrated in **Figure S14a**.⁵⁰ The ^1H -MAS NMR spectra of the treated samples present additional peaks at $\delta = 0.4$ ppm, $\delta = 1.1$ ppm, and $\delta = 3.3$ ppm assigned to the protons in the propylamine chain.⁵¹⁻⁵³ The assignments are illustrated in **Figure S14a**. After reaction with APTES, the silanol peak is shifted to the higher chemical shifts (downfield). The shifting of the peaks is more evident in the treatments 20-24-Ref where a higher density of propylamine groups was obtained. This shifting is a product of the interaction between silanol groups and protonated amines on the surface.^{36,51} Moreover, The propylamine chains are far from each other at low concentrations and they have limited chances to interact with neighbor propylamine chains.¹⁶ On the other hand, the sample reacted with the treatment 20-24-Ref has multiple peaks that can be associated to a second environment. Therefore, propylamine groups can be interacting among each other and with the silica surface leading to multiple environments for some of the protons.^{36,37}

The ^{13}C -CPMAS NMR spectra of the control sample in **Figure 7b** does not show any peak as this does not have propylamine chains on the surface. Three main peaks were identified from the spectrum of the samples treated with APTES. **Figure S14** illustrates the carbon assignments in the propylamine chain. The peak at $\delta = 8.9$ ppm corresponds to the carbon next to the silicium atom, the peak at $\delta = 21.4$ ppm is assigned to the carbon in the middle of the chain, and the peak at $\delta = 41.8$ ppm is for the carbon adjacent to the nitrogen atom.⁵⁴ Interestingly, a second peak near $\delta = 41.8$ ppm is observed in the spectra of samples reacted for 0.5 h. This peak is indicative of a second environment like the one described from the ^1H -MAS NMR results. The

1 relative intensity of the ^{13}C -CPMAS NMR spectrum follows the order 20-24-Ref > 20-0.5-Ref
2 > 20-0.5-RT > 2.5-0.5-Ref. The changes in the relative intensity of the peaks in **Figure 7b** are
3 proportional to the percentages of carbon measured from the elemental analysis in **Figure 6**.
4 Therefore, the signal enhancement is directly related with the abundance of functional groups
5 bonded to the surface of the sample. Additionally, no peaks at $\delta = 18.4$ ppm and $\delta = 58.4$ ppm,
6 associated with ethanol or with ethoxy groups from APTES, were identified in the ^{13}C -CPMAS
7 NMR spectra.³⁵ This means that the APTES is condensed onto the surface thereby forming a
8 covalent bond.

9 The ^{29}Si -CPMAS NMR spectra of the control sample in **Figure 7c** has Q^4 , Q^3 , and Q^2
10 silica groups at the surface assigned to the peaks in the spectrum located at $\delta = -112$ ppm, $\delta =$
11 -101 ppm and $\delta = -90$ ppm respectively.^{51,53,55} The peak shoulder at $\delta = -90$ ppm is more evident
12 in the spectra of functionalized samples because Q^4 and Q^3 reacted with APTES before Q^2
13 silicas, which is to be expected as Q^2 silicas are known for being less reactive than Q^3 .⁵⁶ Also,
14 a new set of peaks in the functionalized samples is observed around $\delta = -60$ ppm, this is
15 assigned to T type silicon similar to the one illustrated in **Figure S14b**. The peaks located
16 around the $\delta = -60$ ppm region are conclusive concerning the formation of a covalent bond
17 between APTES and the silica monolith surface.



1

2 **Figure 7.** Solid state NMR spectra for silica 3D-printed monoliths functionalized with APTES,
 3 ^1H -MAS (a), ^{13}C -CPMAS (b), and ^{29}Si -CPMAS (c). Treatment name listed next to each
 4 spectrum.

5 3.5. Silanization after multiple vacuum wetting

6 Diffusion limitations within the fibers and the monolith resulted in inhomogeneities in
 7 samples 200/150-SC and long reaction times to reach similar carbon and nitrogen contents to
 8 those of the GM in the sample 400/250-SC as seen in **Figure S13a**. Silanization homogeneity
 9 was reached in the samples 200/150-SC and 400/250-SC with the treatment 20-0.5-RT.
 10 However, the extent of functionalization through the monolith was relatively low. In the second
 11 silanization procedure described in the methodology, the treatment 20-0.5-RT was repeated

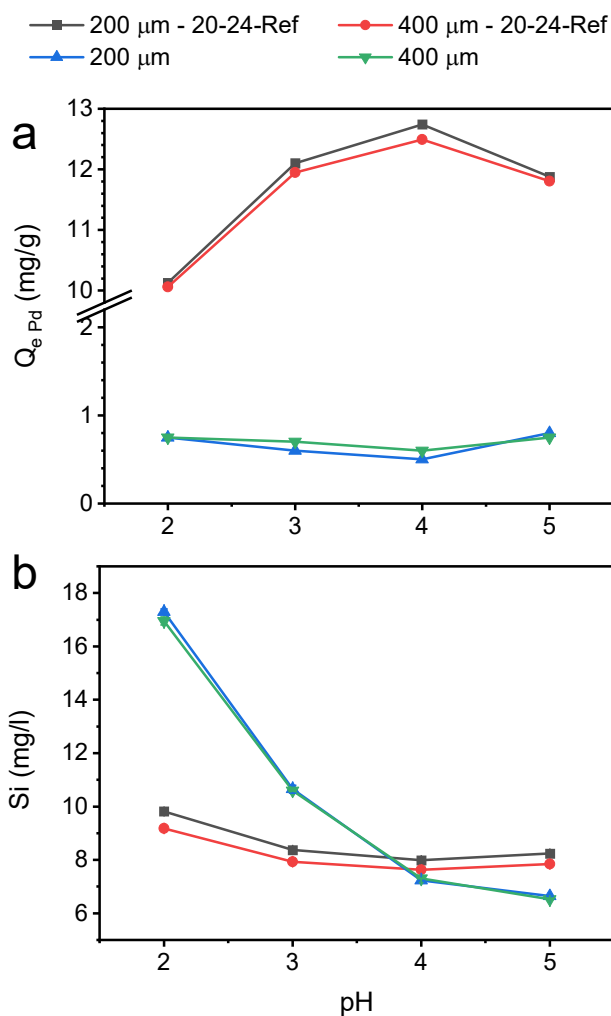
1 three times using 400/250-SC structures to increase the extent of functionalization while
2 assuring homogeneity. After these reaction cycles the carbon content was increased from 0.6
3 wt% to 1 wt% as seen in **Figure 6** for treatment 2.5-0.5-RT and 2.5-0.5-RT-X3 respectively.
4 The 40% increase in carbon and nitrogen content, after three silanization cycles, allows a faster
5 procedure to achieve a homogeneous distribution of the APTES, and a high concentration of
6 APTES on the surface. In fact, 3 cycles of 0.5 h each yielded similar carbon and nitrogen
7 density on the surface as the same reaction run for 17 h (**Figure S13**). This increase in the
8 nitrogen and carbon content is attributed to the bonding of a first layer of APTES which could
9 have a catalytic effect over the bonding of the fresh APTES added in the subsequent vacuum
10 impregnation steps.⁵⁷ In addition, the hydrolysis in the washing step provides new hydroxyl
11 groups that can be used for condensation of the fresh APTES added in the next vacuum
12 impregnation cycle.³⁸

13 **3.6. Adsorption of palladium in functionalized fibers**

14 Palladium adsorption is a well-known application for aminated surfaces, therefore this
15 application was implemented to gather extra information about the availability of the bonded
16 amines for Pd sorption.⁵⁸⁻⁶⁰ The non-functionalized fibers show negligible adsorption
17 capacities, Pd lower than 1 mg/g, in the pH range between 2 and 5 as seen in **Figure 8a**. The
18 functionalized samples have adsorption capacities between 10 and 13 mg/g or 0.094 to 0.122
19 mmol/g. At pH 2 the Q_e of Pd was 20% lower than the same at pH 3, 4, and 5. Q_e for the
20 evaluated silica is comparable with reported values in diverse materials and functional groups,
21 especially with the previous reports using silica as support and 3-propylamine as functional
22 moiety.^{58,61} The result confirms the availability of the amine groups for sorption.

23 Clear differences are observed in the hydrolytic stability between the non-functionalized
24 fibers, and the fibers functionalized with APTES. This was evaluated by measuring the silicium

1 concentration (mg/L) in the solutions after adsorption. **Figure 8b** shows the hydrolytic stability
 2 of the surface at different pH values. From the graph, silicium was detected in all the solutions
 3 after adsorption by the silica materials. The non-functionalized fibers have a significant
 4 degradation at pH 2 and pH 3 compared with the fibers functionalized with the treatment 20-
 5 24-Ref. A previous study demonstrated that at pH values below 3 the amine groups are
 6 protonated, and therefore the attacks over the surface do not occur extensively.³⁷ At pH 4 the
 7 content of silicium was similar for the functionalized and non-functionalized fibers. Finally, at
 8 pH 5 the non-functionalized samples perform better regarding silicium leaching compared to
 9 the functionalized fibers. Although the reasoning of this behavior is unknown, and at pH 5 the
 10 amines are still protonated, it is clear that propylamine groups on the surface of silica promote
 11 silica solubilization even at an acidic pH.³⁷



1 **Figure 8.** Impact of the pH on the adsorption capacity for Pd (mg/g) between pH 2 to 5 for
2 fibers of 200 μm and 400 μm before and after the silanization with the treatment 20-24-Ref.
3 (a) Residual Si concentration (mg/L) in solution (b), after stirring Pd solutions of 150 mg/L for
4 24 h with 200 mg of 200 μm and 400 μm fibers before and after functionalization with the
5 treatment 20-24-Ref. The lines are for visual reference and do not represent a model.

6 **4. Conclusion**

7 The homogeneity of functional groups on the surface of 3D-printed porous silica structures was
8 investigated after silanization in a batch reactor. The results demonstrate that APTES can be
9 covalently bonded to the surface and homogeneously distributed in 3D-printed silica monoliths
10 with gap-spanning architectures that have interfiber distances greater than 250 μm . In addition,
11 the extent of functionalization is dependent on fiber diameters above 359 μm and is
12 independent of the configuration of the internal structure. Consequently, the reaction in vessels
13 has high potential for applications where a large geometric surface area is not required, such as
14 those with pressure drop limitations. However, challenges remain to achieve a homogeneous
15 functionalization in structures with smaller interfiber distances. Alternative silanization
16 protocols must be developed, aiming at the minimization of the mass diffusion limitations
17 observed in the present study.

18 Multiple silanization cycles with vacuum impregnation and shorter reaction times yielded
19 a higher extent of functionalization and a homogeneous distribution of the monoliths. The first
20 layer of APTES is homogeneously distributed within the monolith. Subsequent reaction cycles
21 allow the increase of the extent of functionalization as the first layer of bonded APTES has
22 new hydroxyl groups which can be condensed with fresh APTES from the next silanization
23 cycle enhancing the extent of functionalization while retaining the homogeneity of amine
24 groups throughout the monolith.

1 This study is a baseline for functionalization of 3D-printed complex structures using batch
2 reactors and demonstrates that fibers functionalized with propylamine groups are available for
3 Pd adsorption. In addition, the concentration of amine groups in the reported structures is
4 enough to achieve hydrolytic stability at pH values lower than 4. Further research aiming at the
5 effective use of the monoliths in metal sorption or other applications will be focus on the
6 increase of the specific surface area to allow a higher amount of functional groups and in the
7 development of grafting protocols for higher geometric surface areas.

8

9 **Supporting Information**

10 **Figure S1.** Top layer of 3D-printed monoliths, simple cubic, and face-centered cubic
11 configurations

12 **Figure S2.** Particle size distribution of a monolith ground with a mortar

13 **Figure S3.** Monolith divided between core and walls

14 **Figure S4.** Elastic modulus and shear stress for samples mixed during different times

15 **Figure S5.** Optical microscopy of the extruded fibers

16 **Figure S6.** Optical microscopy of cross sections from the monolith 400/250-SC

17 **Figure S7.** Optical microscopy of cross sections from the monolith 200/150-SC

18 **Figure S8.** Microstructure of the fibers analyzed by SEM-EDX

19 **Figure S9.** Nitrogen sorption and BJH Pore size distribution

20 **Figure S10.** Pore size distribution calculated from mercury intrusion

1 **Figure S11.** Thermogravimetry measured in segmented samples before and after silanization
2 with APTES

3 **Figure S12.** First derivative of the weight loss and mass spectroscopy for walls after treatment
4 with 20-24-Ref

5 **Figure S13.** Kinetics of functionalization with APTES in SiO₂ monoliths

6 **Figure S14.** Solid state NMR assignments

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10 **Notes**

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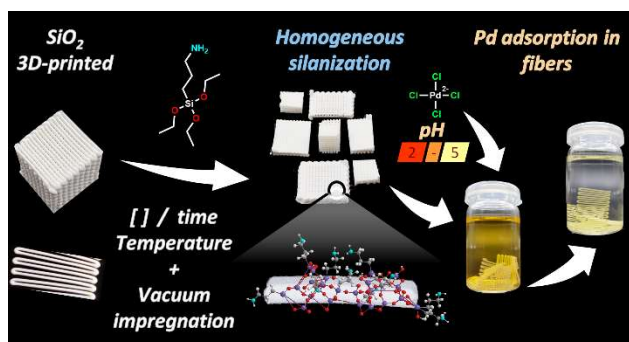
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18 **Graphical abstract**



1

2 Caption: Homogeneity and extent of silanization on 3D-printed silica structures were evaluated
 3 using 3-aminopropyltriethoxysilane. The extent of functionalization does not have differences
 4 for fibers below 400 μm . Vacuum impregnation and short reaction times provide
 5 homogeneously functionalized structures. The extent of functionalization was increased by
 6 doing multiple cycles. On the other hand, a single cycle leads to inhomogeneous
 7 functionalization for structures with interfiber distances below 250 μm . Functionalized fibers
 8 were effective adsorbing palladium in acid solutions. In addition, the functionalized material
 9 showed neglectable solubility its low pH values.

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