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Flash co-pyrolysis of biomass with polylactic acid

part 1. Influence on bio-oil yield and heating value

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Abstract

High amounts of water present in bio-oil are one of the major drawbacks for its utilisation as a fuel. One technology that shows the potential to satisfy the demand for bio-oil with a reduced water content is the flash co-pyrolysis of biomass with polylactic acid, PLA. The influence of PLA on the pyrolysis of willow is investigated with a semi-continuous home-built pyrolysis reactor. Flash co-pyrolysis of willow/PLA blends (10:1, 3:1, 1:1 and 1:2) show synergetic interaction. A higher bio-oil yield and a lower water content as a function of the willow/PLA ratios are obtained. Among the tested blends, the 1:2 willow/PLA blend shows the most pronounced synergy: a reduction in the production of pyrolytic water of almost 28 %, accompanied by an increase of more than 37 % in the production of water-free bio-oil. Additionally, PLA shows to have a positive influence on the energetic value of the bio-oil produced and on the resulting energy recuperation.

Key words: flash co-pyrolysis; willow; polylactic acid; pyrolytic water; bio-oil.

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1. Introduction

Global Warming, the Kyoto Protocol, the emission of greenhouse gases and the depletion of fossil fuels are the topics of environmental pleadings worldwide. The development of new and renewable energy sources (including biofuels) is the key to change [1]. The flash pyrolysis of biomass is a promising route with regard to the production of solid (char), liquid (bio-oil) and gaseous materials as possible alternate energy sources [2-4]. In order to maximise the bio-oil yield, process conditions should be: low temperature, high heating rate and short gas residence time [5, 6]. Today, bio-oil can substitute fuel oil or diesel in many static applications including boilers, furnaces, engines and turbines used for electricity generation. Additionally, it can be upgraded to transportation fuels [7] and even to chemicals with added value.

The flash pyrolysis of biomass inherently results in the production of pyrolytic water, which is one of the major drawbacks of the bio-oil produced. Nevertheless, the presence of water has both positive and negative effects on the bio-oil properties [5, 8]. It improves bio-oil flow characteristics, which is beneficial for combustion. Moreover, it leads to a more uniform temperature profile in the cylinder of a diesel engine and to lower NO_x emissions. On the other hand, it lowers the heating value and flame temperature of the bio-oil. It also contributes to the increase in ignition delay and in some cases to the decrease of combustion rate as compared to diesel fuels. The reduction of the water content is one of the few required but essential upgrading steps in order to increase the applicability of bio-oil and to make the production of bio-oil competitive. Oasmaa summarised the requirements of bio-oil set by Ensyn (a liquid producer), Wärtsilä (an engine manufacturer) and Birka (a potential bio-oil user). Here, the maximum water content was defined as 25 - 26 wt. % [9], while literature reports a water content between 15 – 30 % and even more [6, 8].

To our knowledge, the flash pyrolysis of willow has not been investigated extensively yet. Ingemarsson studied the slow pyrolysis of willow and analysed the compounds produced using gas chromatographic

methods [10]. Mészáros et al. performed TG/MS analysis of willow and other young wood samples in order to obtain information on their thermal behaviour [11]. Prins et al. specifically addressed the decomposition of hemicellulose of willow in the relatively low temperature range of 498 – 573 K, a process also known as torrefaction [12, 13].

The use of co-pyrolytic techniques on biomass/plastic ratios has already been investigated [14-17]. One of the most important parameters for liquid production is the ratio in the feedstock.

Polylactic acid, PLA, is a biologically degradable polymer and is produced principally via microbial fermentation of sugar feedstock [18]. PLA is possibly the most commonly applied biopolymer and has the most potential for widespread use, but does not have the best biodegradability properties amongst biopolymers. Therefore, co-pyrolysis of PLA and biomass (willow) offers an alternative waste treatment option and may act as an upgrading step during the pyrolysis of willow. The thermal decomposition of PLA has already been studied in detail [19-22].

The goal of the present research is to reduce the amount of pyrolytic water by flash co-pyrolysis of willow and PLA. Therefore, the co-pyrolytic behaviour of the willow/PLA blends are investigated with a semi-continuous home-built pyrolysis reactor. In this paper, the influence of PLA and willow on the bio-oil yield, its water content and heating value during flash co-pyrolysis will be discussed.

2. Experimental

2.1. Materials

The experiments are performed on willow - *Salix*, PLA and willow/PLA blends. The willow branches (the leaves are not taken into account in this study) are cut and dried at room temperature before being shredded into small particles (~2mm). A particle size of < 2mm guarantees a fast inner-heating rate during pyrolysis and thus ensures a flash pyrolysis of the entire particle.

The experiments on willow/PLA blends with a w/w ratio of 10:1, 3:1, 1:1 and 1:2 are investigated and compared with the results obtained for 100% willow and 100% PLA (reference samples 1 and 2, respectively) to evaluate the effects on the bio-oil yield, its water content and its calorific value.

2.2. Explorative analysis of pure biomass and PLA

Ultimate Analysis

The CHNS- and O-content of the input materials are determined via two distinct experiments, using a FlashEA 1112 Elemental Analyser of Thermo Electron Corporation. Approximately 2 – 4 mg of sample is introduced into a container, which is injected by an autosampler. In case of CHNS-determinations, 5 – 10 mg vanadiumpentoxide is added to the sample as a combustion catalyst. 2,5-Bis(5-tert-butyl-benzoxazol-2-yl)thiophene (BBOT) and L-cystine are used as standards for the CHNS- and O-determinations, respectively.

Thermogravimetric analysis - TGA

About 30 mg of sample is pyrolysed under approximately 35 ml/min N₂ flow at a heating rate of 10 K/min from room temperature (RT) to 973 K with a DuPont Instruments 951 Thermogravimetric Analyzer.

Thermogravimetric/Mass spectrometric analysis - TG/MS

A Hi-Res TGA 2950 Thermogravimetric Analyzer of TA Instruments is connected with a Pfeiffer Vacuum ThermoStar mass spectrometer. Approximately 1 – 2 mg of sample is pyrolysed under a Helium flow of 100 ml/min at a heating rate of 20 K/min from RT to 873 K. The mass spectrometer is set at the standard ionising voltage of 70 eV with a mass range m/z of 5 – 255 and a scan rate of 5 scans/min.

Thermogravimetric/Fourier Transform – Infrared analysis - TG/FTIR

A DuPont Instruments 951 Thermogravimetric Analyzer, interfaced (at 473 K) with a gas cell, and coupled with a Bruker Vertex 70 FT-IR spectrometer (resolution: 4 cm⁻¹) is applied. Approximately 20 mg of sample is pyrolysed at a heating rate of 20 K/min from RT to 873 K under a constant Helium flow of 100 ml/min.

2.3. Flash Pyrolysis

Experimental flash pyrolysis set-up

The semi-continuous home-built pyrolysis reactor (360 mm high with a diameter of 88 mm), Fig. 1 (part a), is manufactured in stainless steel (AISI 304). Within the reactor, a heat transfer medium (white sand, \pm 700 g or 450 ml) is inserted. Before use, this sand is dried at 383 K to ensure that all water is removed. Preliminary, the sand is pre-treated in batch at 873 K to remove all impurities. During the entire process, the sand is in constant motion with the aid of an Archimedical screw, ensuring a homogeneous temperature sand bed operating system. This Archimedical screw also serves as a gas inlet system. The reactor (and the sand) is heated by a tailored heating jacket (Horst GmbH, Lorsch, Germany).

The injection system, Fig. 1 (part b), is manufactured in stainless steel (AISI 304) as well. It consists of a reservoir with a volume of 600 ml and an injector. The injector is a hollow tube linking the reservoir, which contains the biomass, with the reactor. Via this tube, the biomass is transported into the reactor by means of a second Archimedical screw with a controlled feeding rate (1 – 120 rpm). A second gas inlet is situated inbetween the biomass container and the injector.

The recuperation system, Fig. 1 (part c), is a stainless steel (AISI 304) collector vessel with a volume of 580 ml and is kept at room temperature. Inbetween the reactor and the collector, a small water cooler is constructed to quench the gases. On top of the collector vessel, a cold trap made out of copper (kept at

77 K with liquid nitrogen) is installed to collect all condensable gases. The non-condensable gases exit the recuperation system via the chimney into a fume hood.

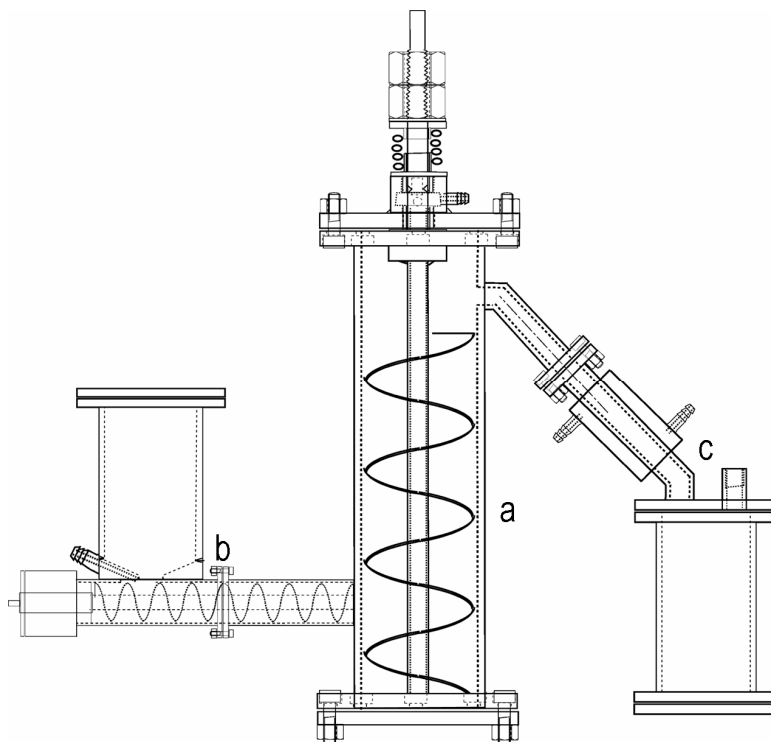


Figure 1: Pyrolysis set-up: a, reactor (at PT in K); b, injection system (at RT in K) with a biomass reservoir; and c, recuperation system (at RT in K) with an additional water cooler.

Procedure

Preliminary, all materials (± 700 g sand and ± 100 g input) are dried at 383 K. When heating has started, nitrogen gas continuously enters the reactor via two ways to guarantee an “oxygen-free” environment: firstly, via the hollow shaft of the Archimedical screw in the reactor which also acts as a gas pre-heater (70 ml/min), and secondly via the injection system (70 ml/min). As soon as the sand inside the reactor reaches the pyrolysis temperature (PT), the nitrogen flow is stopped and the injection system is started; inserting the willow, PLA or willow/PLA blend into the reactor at a rate of 20 rpm, which is, at the moment, the optimal speed for the material in question. In this way, an injection rate of approximately 140 ml per minute is achieved. The willow, PLA or willow/PLA blend subsequently undergoes a flash pyrolysis and is converted into volatiles which mainly condense into the recuperation system as bio-oil.

During the entire experiment (heating, injection, pyrolysis,...), temperature measurements are taken at the top of the sand bed with a thermocouple type K.

2.4. Water content and heating value of bio-oil

Water content

The water content of the different bio-oil samples, containing a high percentage of water, is measured using the Dean-Stark method. Around 5 to 10 ml bio-oil is introduced into a 250 ml flask together with approximately 60 ml toluene. Water is separated from the bio-oil in azeotropic conditions into a calibrated reservoir, indicating the amount of water present in the bio-oil.

Bio-oils with very low water content are analysed by means of a Karl-Fisher titration. A SCHOTT, equipped with a TR85 detector, a 180/10 full-automatic burette and a TM120 reaction vessel, is used. Here, experiments are performed on 0.5 ml bio-oil.

Calorimetry

The samples (approximately 1 g) are analysed with an IKA C5003 control calorimeter equipped with an IKA KV 600 Digital water cooler and a Sartorius CP224S analytical balance. Oxygen is connected to the system to pressurise the bomb. Measurements are executed in dynamic mode and the calibration of the system is performed with benzoic acid (palleted, C723) of IKA with a higher heating value (H.H.V.) of 26460 J/g (relative standard deviation of 0.01%).

3. Results and discussion

The main characteristics of willow and PLA are listed in Table 1. Based on the ultimate analysis, both materials have a high C- and O-content, and a low H-content. No S is detected and the N-content is

very low. Their calorific values have been measured as well and are within the same range, around 19000 J/g.

Table 1: Main characteristics (on dry basis) of willow and PLA.

<u>Characteristics</u>	<u>Willow</u>	<u>PLA</u>
<u>Proximate analysis (%)</u>		
Moisture	3.24	0.00
Volatile	74.66	98.05
Fixed C	20.39	1.30
Ash	1.71	0.65
<u>Ultimate analysis (%)</u>		
Carbon	46.91	49.84
Hydrogen	5.95	5.63
Nitrogen	0.63	0.15
Oxygen	41.69	44.42
H/C molar ratio	1.52	1.36
O/C molar ratio	0.67	0.67
<u>Calorific value (J/g)</u>		
Calorimetric analysis	19088	18597

TGA is executed to obtain an overview of the basic characteristics (Table 1) and insight in the pyrolysis behaviour of willow, PLA and their blends. For the pyrolysis of the pure materials and the 1:2 blend, the mass loss curves and the derivatives are shown in Figure 2. The thermogram of willow points out that willow contains more than 3% moisture, while for PLA a negligible amount is measured.

Willow, a woody biomass, mainly consists of the three basic constituents of wood: cellulose, hemicellulose and lignine. It is known that lignin decomposes within a wide temperature interval (433 – 1173 K) and its DTG peak is not commonly distinguishable [11, 12, 23]. Hemicellulose (the shoulder in the profile of Fig. 2a) is the second constituent to decompose, followed by cellulose (the main DTG peak centered around 626 K), which decomposes in a narrow temperature interval from about 473 up to 673 K. This is the interval in which the main decomposition takes place and which accounts for the greatest mass loss during the biomass pyrolysis process [11, 12, 23]. PLA on the other hand (Fig. 2b) decomposes in one single and narrow temperature interval that ranges from 563 to 663 K, with a maximum at 632 K. Important to note is that the maximum decomposition temperature of willow and PLA coincide.

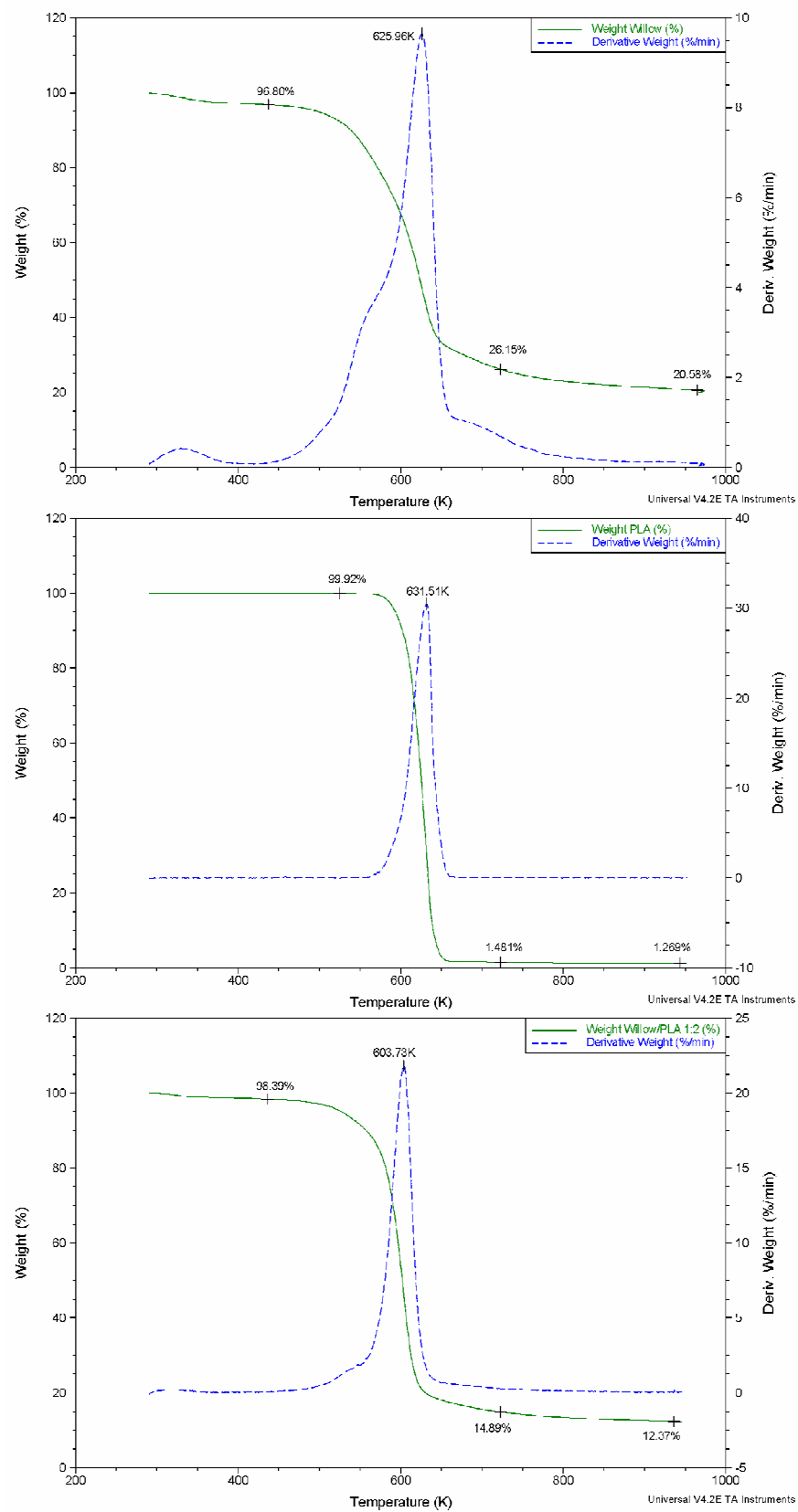


Figure 2: Weight loss and their derivatives of a, willow; b, PLA; and c, 1:2 willow/PLA, obtained by TGA.

The triple stage decomposition of willow is observed in all blends, however, in reduced form directly correlated with the addition of PLA. The thermogram of the 1:2 willow/PLA blend gives a profile that is very comparable to that of pure PLA (Fig. 2c). The peak maxima of the derivatives of the pure materials and their blends ranges between 603 K and 633 K. Figure 2 also shows that most of the decomposition reactions are finalised at a temperature of about 673 K, justifying a maximum flash pyrolysis temperature of 723 K during the semi-continuous pyrolysis experiments.

Based on the TG/MS ion-kinetograms of m/z 18 (Figure 3), it can be concluded that pyrolytic water is formed during the intense decomposition at the temperature range between 473 and 673 K. More specifically, the pattern of the DTG-curves in the thermogram (Fig. 2) are also visible for the evolution of mass '18' (water) in function of time during the pyrolysis of willow, PLA, and their blends (Fig. 3). A difference in the amount of pyrolytic water produced from pure willow (1 g of starting material) and pure PLA (also 1 g of starting material) is observed, predicting a high and a low water content for willow and PLA bio-oil, respectively. Additionally, an intermediate production of pyrolytic water for the 1:2 willow/PLA blend (2 g of starting material) is indicated.

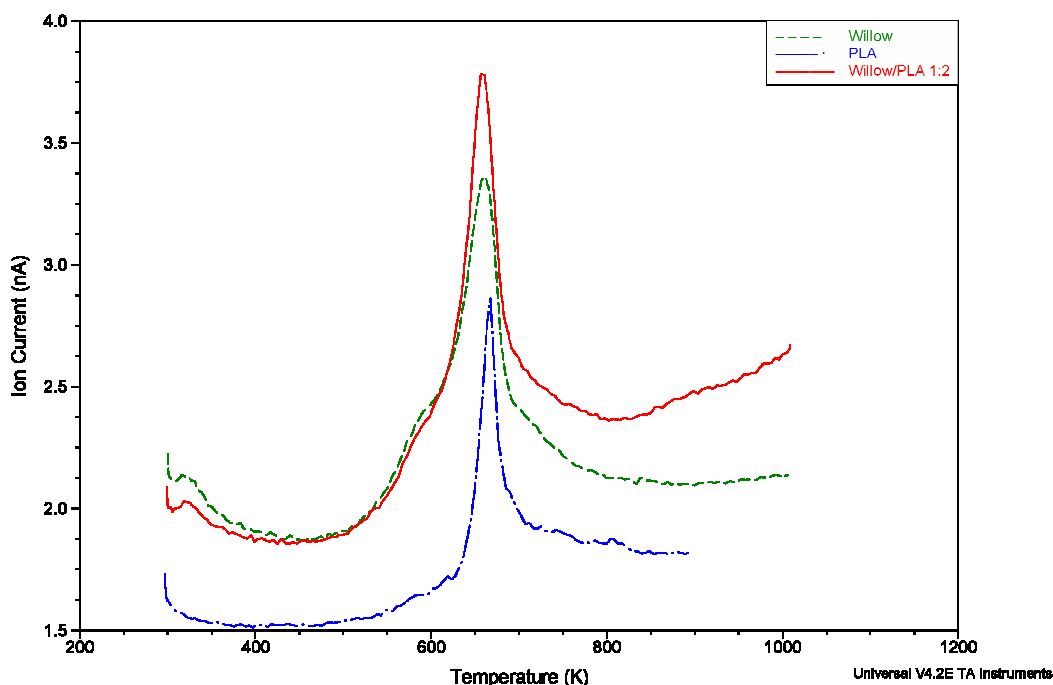


Figure 3: Evolution of mass '18' in function of temperature (= ion-kinetogram of m/z 18) for willow, PLA, and 1:2 willow/PLA, obtained by TG/MS.

Other masses, e.g. m/z 16, 28, 29, 44, 45, and 46; potentially representing the release of methane, carbon monoxide, aldehydes and/or ketones, carbon dioxide, alcohols and/or ethers, and acids respectively, have additionally been detected by means of TG/MS. Here, no extra conclusions could be drawn besides the fact that the evolution of the ion-kinetograms resembles the pyrolysis DTG-curves, as is shown for water in Figure 3.

TG/FTIR analysis shows some other interesting evolutions during co-pyrolysis. For comparison, the FT-IR spectra extracted at the highest pyrolysis decomposition rate ($T = 603 - 633$ K) are visualised in Figure 4. First, a shift in the most abundant band at $1650 - 1860$ cm^{-1} , which represents the carbonyl functionalities, is observed. Here, a shift of band position towards a higher wavenumber is shown: 1745 cm^{-1} for willow, 1766 cm^{-1} for PLA and 1793 cm^{-1} for 1:2 willow/PLA. Additionally, an intense peak at $1200 - 1250$ cm^{-1} for 1:2 willow/PLA is formed and cannot be explained by the reference materials according to the applied ratio. Finally, the ratio between the CO and the CO_2 bands for willow, PLA and 1:2 willow/PLA varies (Fig. 4): in the case of PLA, the CO band ($2000 - 2200$ cm^{-1}) is larger compared with the CO_2 band ($2300 - 2400$ cm^{-1}), while the CO band is clearly less intense for willow and for 1:2 willow/PLA compared with their CO_2 band, although the 1:2 blend is dominated by PLA. Such differences in pattern can only be explained by additional reactions occurring during co-pyrolysis, resulting in an altered gas composition (both condensable and non-condensable). Figure 5 shows the evolution of CO and CO_2 during the thermal decomposition of willow, PLA and 1:2 willow/PLA in more detail. The response for CO_2 between 473 and 623 K varies in importance relative to the maximum decomposition temperature (> 623 K): PLA shows almost no response before 623 K, while willow shows an important shoulder in this temperature interval. Even though the proportion between CO and CO_2 of the 1:2 blend resembles willow the most ($\text{CO}_2 \gg \text{CO}$), the evolution of CO_2 obviously differs from that of willow showing only a negligible shoulder between 473 and 623 K. This indicates that another degradation mechanism takes place and confirms the occurrence of additional reactions during co-

pyrolysis. It seems that the degradation of 1:2 willow/PLA is shifted towards higher temperatures in comparison with pure willow.

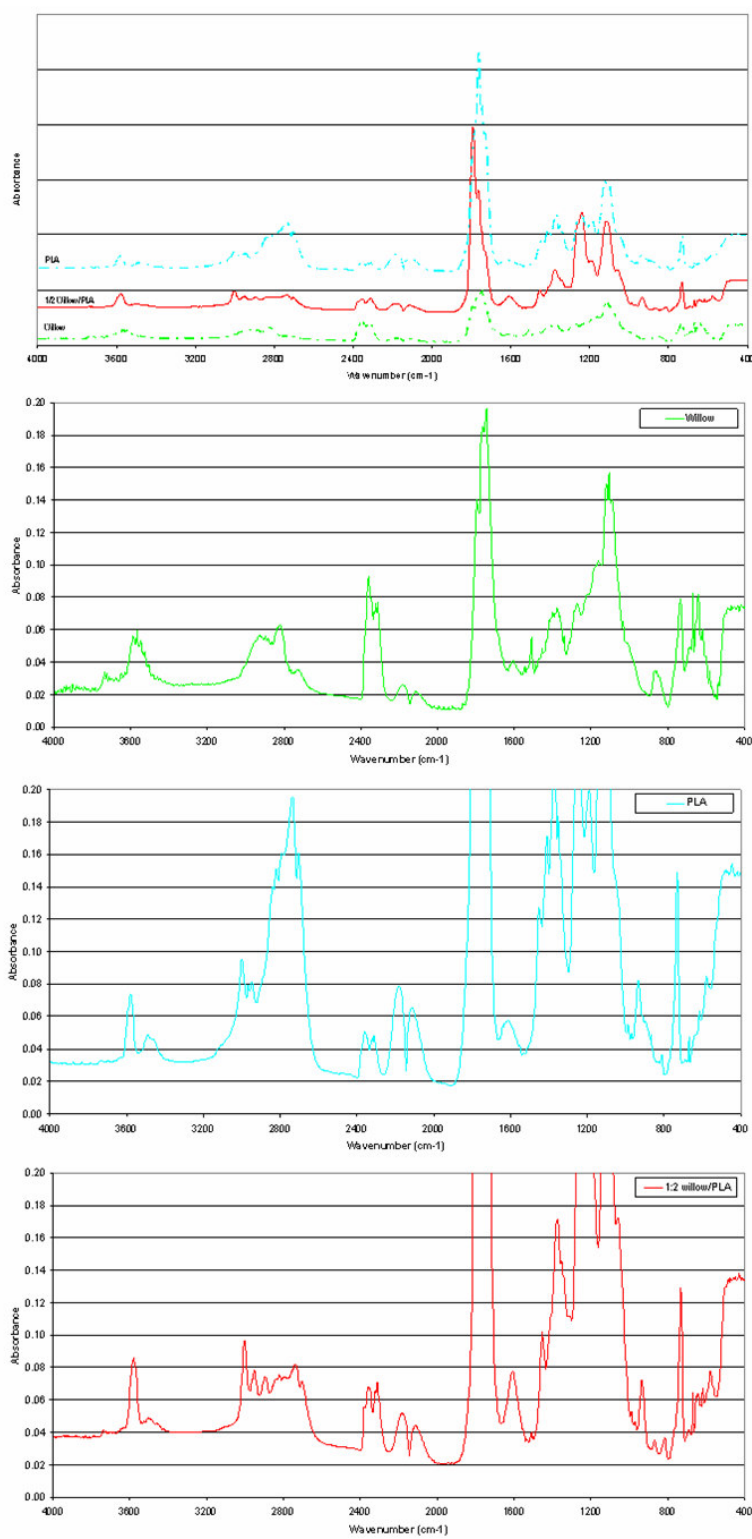


Figure 4: FT-IR spectra of the evolving gases at the maximum decomposition rate during pyrolysis; a, overlay; b, for willow; c, PLA (scaled up); and d, 1:2 willow/PLA (scaled up), obtained by TG/FTIR.

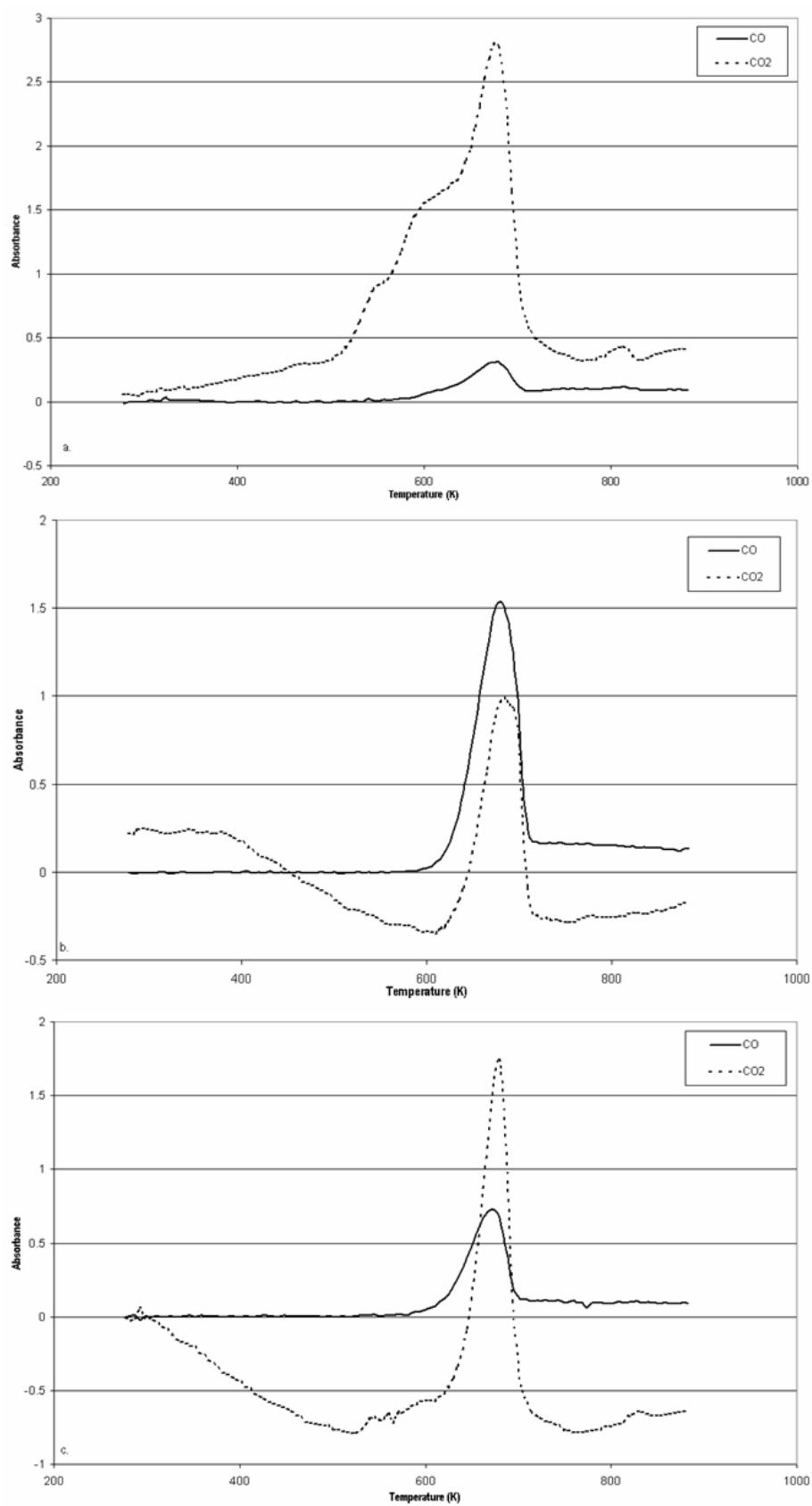


Figure 5: The evolution of CO and CO₂ during the thermal decomposition of a, willow; b, PLA; and c, 1:2 willow/PLA, obtained by TG/FTIR.

The 3D diagrams in Figure 6, which plot the absorbance (Y) in function of wave number (X) and temperature (Z), obtained by TG/FTIR show that carbonyl functionalities ($1650 - 1860 \text{ cm}^{-1}$) are the most important functionalities in the evolving gases of all three samples during pyrolysis, representing the most abundant peak in the diagrams. Additionally, the evolution of functional groups, expressed as the overall intensity within a specific spectral window, as a function of temperature, has been investigated. Figure 7 shows the evolution of carbonyl functionalities within the $1650 - 1860 \text{ cm}^{-1}$ range, and of esters and -C-O- stretching within the $950 - 1500 \text{ cm}^{-1}$ range. With regard to the carbonyl functionalities (Figure 7 - a), the most abundant peak is obtained from PLA, and the least abundant from willow, while the 1:2 blend is situated somewhere inbetween. The same observation is made for methane and is expected to occur for all functionalities. However, in case of the esters and -C-O- stretching range the 1:2 willow/PLA blend seems to represent the most abundant peak (Figure 7 - b). This observation confirms that additional reactions take place during co-pyrolysis of willow and PLA, resulting in an altered gas composition. Moreover, Figure 7 also indicates that the start of the decomposition of the blend is shifted towards higher temperatures compared to pure willow.

Due to the fact that biomass, and more specifically willow, decomposes in three stages, some possible general reactions can be proposed: 1. the decomposition of lignine and/or hemicellulose results in volatiles which react with PLA, which on its turn can additionally react with cellulose; 2. the decomposition of willow (cellulose, hemicellulose and/or lignin) and PLA takes place simultaneously, resulting in 2.a. interactions during the decomposition of willow and PLA and/or 2.b. interactions between volatiles after decomposition of willow and PLA and/or 2.c. interactions between condensables of willow and PLA.

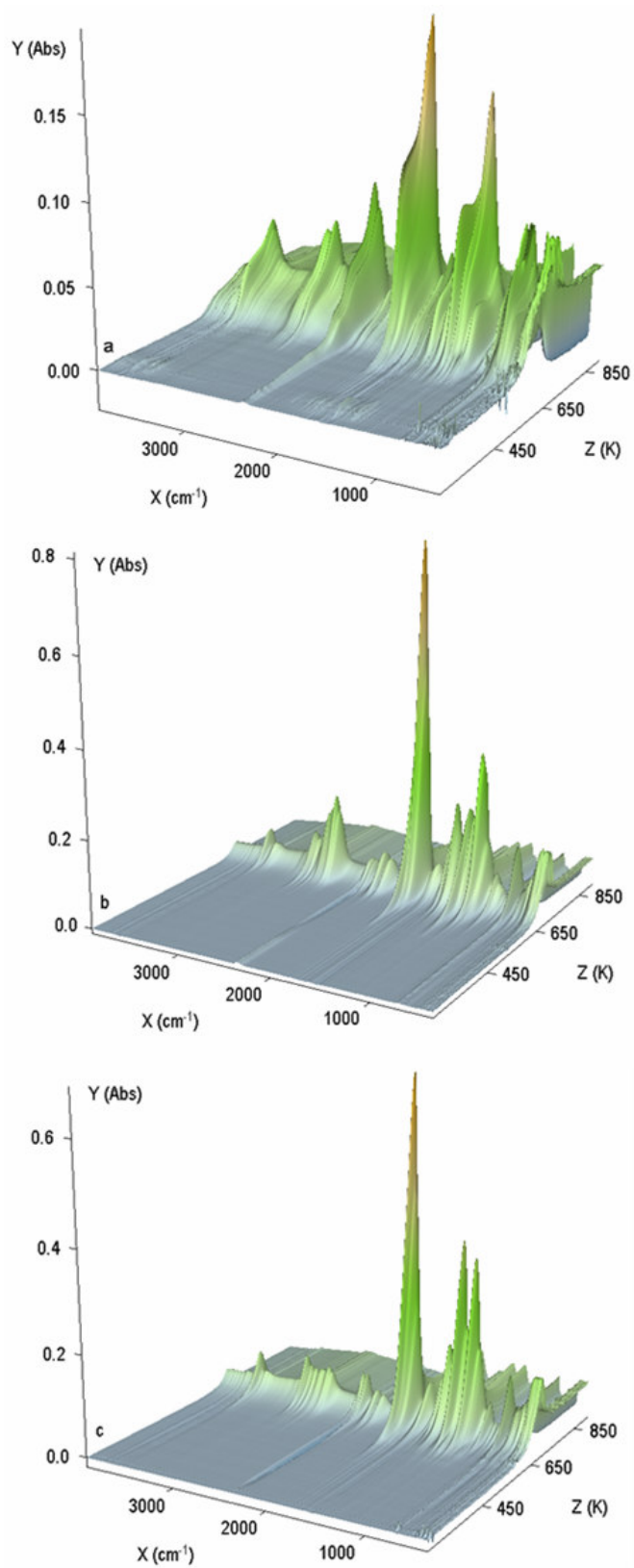


Figure 6: 3D diagrams of a, willow; b, PLA; and c, 1:2 willow/PLA with X: Wave number (cm^{-1}); Y: Absorbance Units (Abs); Z: Temperature (K), obtained by TG/FTIR.

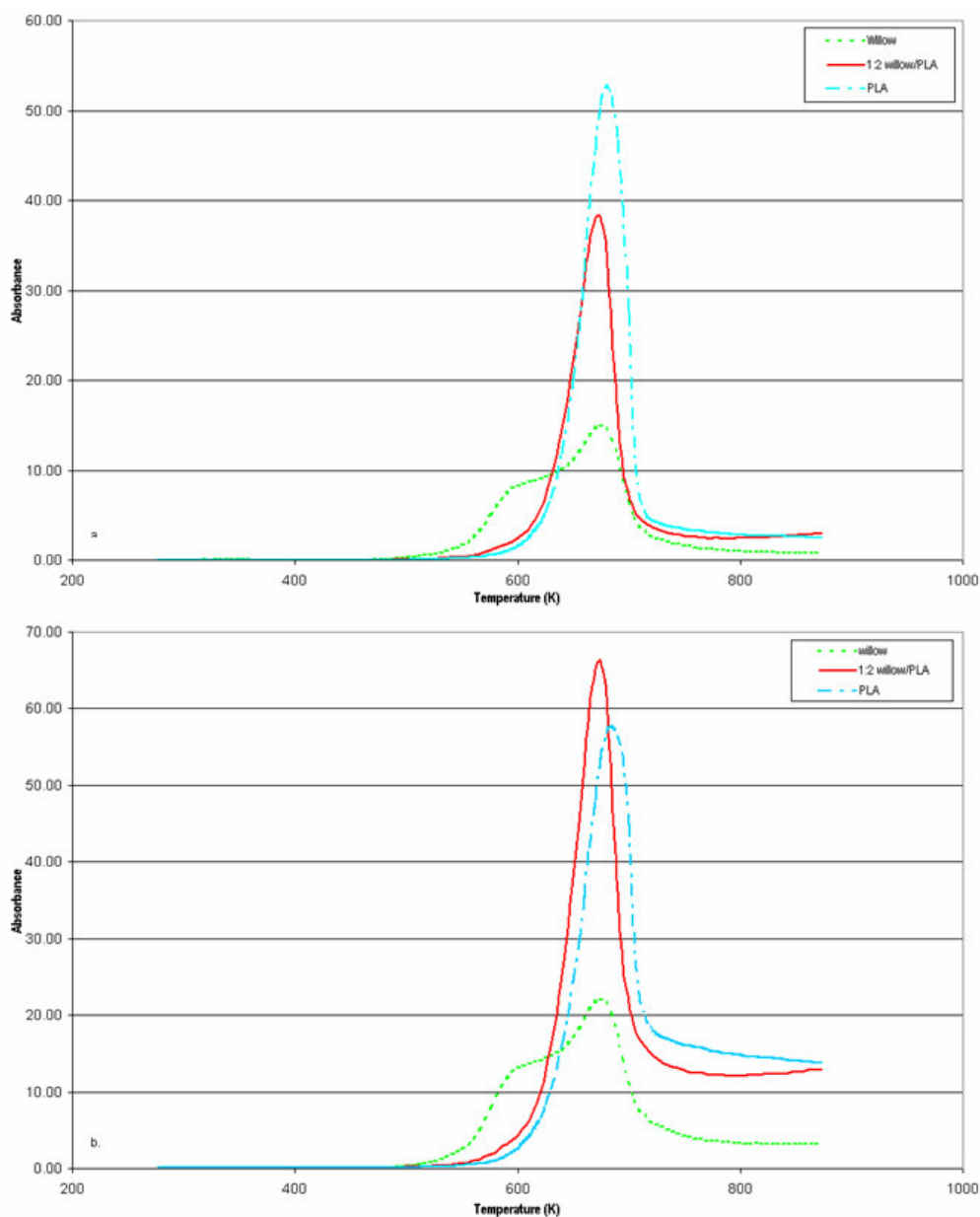


Figure 7: Traces of a, carbonyl functionalities; and b, esters and -C-O- stretching; for willow, PLA, and 1:2 willow/PLA, obtained by TG/FTIR.

Based on the above observations and the proposed reaction mechanisms, flash pyrolysis is performed at 723 K on pure willow, pure PLA, and 4 different w/w ratios (10:1, 3:1, 1:1 and 1:2) of willow/PLA-blends. Table 2 gives a brief summary of the pyrolysis yields and efficiencies of the bio-oil, char and gas productions. The amount of gases is calculated by difference. In Table 3 a subdivision of bio-oil into water-free bio-oil and pyrolytic water is made.

Table 2: Pyrolysis yields and efficiencies of the bio-oil, char and gas productions.

	<u>Willow</u>	<u>10:1</u>	<u>3:1</u>	<u>1:1</u>	<u>1:2</u>	<u>PLA</u>
<i>Input (m%)*</i>						
Willow	100.0	91.3	75.4	51.8	34.6	0.0
PLA	0.0	8.7	24.6	48.2	65.4	100.0
<i>Output (m%)</i>						
Bio-oil	48.85	50.90	52.70	51.30	55.53	40.60
Char	23.20	20.1	17.1	13.3	n.a.**	1.5
Gases (by diff.)	27.95	29.0	30.2	35.4	n.a.***	57.9

*Input (m%) is calculated on dry basis.

**The amount of char is unknown due to a failure during sample preparation.

***The amount of gases is calculated by difference, which is impossible to calculate for the 1:2 blend due to missing data (amount of char).

In Table 2, a first indication towards synergy is observed: the co-pyrolysis of PLA and willow results in a higher bio-oil yield compared to the sum of the fractional experimental values of both inputs. The synergy seems to increase in direct proportion to the addition of PLA. This synergistic effect is confirmed in Table 3, where the production of water-free bio-oil is higher and that of pyrolytic water lower compared to the sum of the fractional experimental values of both inputs. So, the addition of PLA results into an enhanced bio-oil and water-free bio-oil yield, and a lower water content. The lower water content is a result of the more pronounced decrease in the production of pyrolytic water than theoretically would be expected (except for the 10:1 blend).

Table 3: Subdivision of bio-oil into water-free bio-oil and pyrolytic water based upon the water content; obtained out of 100 g input.

	<u>Willow</u>	<u>10:1</u>	<u>3:1</u>	<u>1:1</u>	<u>1:2</u>	<u>PLA</u>
Bio-oil (g)	48.85	50.90	52.70	51.30	55.53	40.60
<i>Water content (m%)</i>	36.46	34.1	25.6	15.5	8.3	0.8
Water-free bio-oil (g)	31.04	33.54	39.23	43.33	50.93	40.28
Pyrolytic water (g)	17.81	17.36	13.47	7.97	4.60	0.32

The synergy reaches its maximum for the 1:2 willow/PLA blend and is observed in two distinct areas:

- firstly, a higher bio-oil yield (Table 2), i.e. + 28 % more bio-oil versus the theoretical valueⁱ,
- and secondly, a lower water content (Table 3), i.e. – 37 % less water versus the theoretical valueⁱⁱ.

ⁱ The theoretical bio-oil yield = $[(34.6\text{g} \times 48.85\% + 65.4\text{g} \times 40.60\%)/100] = 43.45\text{ m\%}$, while the actual bio-oil yield is 55.53 m%, thus an increase of 12.08 m% or $[(12.08 \times 100)/43.45] = + 27.8\%$.

ⁱⁱ The theoretical water content = $[(34.6\text{g} \times 36.46\% + 65.4\text{g} \times 0.8\%)/100\%] = 13.1\text{m\%}$, while the actual water content of the bio-oil is 8.3 m%, thus a decrease of 4.8 m% or $[(4.8 \times 100)/13.1] = - 36.8\%$.

Incorporating both observations in view of the water-free bio-oil yield, an increase of 37 % is obtained as a synergetic effect, which is clearly substantial both quantitatively and qualitativelyⁱⁱⁱ.

The averaged experimental H.H.V.'s obtained by calorimetry are summarised in Table 4 and show a relative standard deviation of maximum 1 %. The addition of PLA clearly shows a third advantage, namely an increase in the H.H.V. of bio-oil produced from willow/PLA blends compared to bio-oil of pure willow (16128 J/g to 19697 J/g). However, bio-oil of pure PLA has the highest H.H.V. (22217 J/g). The main reason for the increase in H.H.V. seems to be the decrease of the water content.

Table 4: H.H.V.'s of input materials and bio-oils in Joule per gram.

<u>Sample</u>		<u>HHV (J/g)</u>
Input*	Willow	19088
	PLA	18597
Bio-oil	Willow	16128
	Willow/PLA 10:1	16832
	Willow/PLA 3:1	17683
	Willow/PLA 1:1	18489
	Willow/PLA 1:2	19697
	PLA	22217

*The HHV of the input materials are calculated on dry basis.

Taking into account the bio-oil yield, the experimental H.H.V. of the 1:2 willow/PLA bio-oil can be translated into an energy recuperation of 58 %^{iv}, while bio-oils from pure willow and pure PLA show an energy recuperation of only 41 % and 48.5 %, respectively. In this case, a synergy of 27 % is calculated^v, making the co-pyrolysis of willow and PLA an energetically and economically attractive route to pursue.

ⁱⁱⁱ The theoretical water-free bio-oil yield = $[(34.6g \times 31.04\% + 65.4g \times 40.28\%)/100\%] = 37.08m\%$, while the actual water-free bio-oil yield is 50.93 m%, thus an increase of 13.85 m% or $[(13.85 \times 100)/37.08] = + 37.34 \%$.

^{iv} The energy recuperation (in bio-oil) = $[(55.53g \times 19697J/g) \times 100/(34.6g \times 19088J/g + 65.4g \times 18597J/g)] = 58.28\%$ for the 1:2 willow/PLA co-pyrolysis.

^v The theoretical energy recuperation = $[(34.6g \times 41.27\% + 65.4g \times 48.50\%)/100] = 46.00 \%$, while the actual energy recuperation is 58.28 %, thus an increase of 12.28 % or $[(12.28 \times 100)/46.00] = + 26.7 \%$.

4. Conclusions

With the aid of TG, TG/MS and TG/FTIR, the decomposition of the input materials over a broad temperature range is visualised. Besides a reduction in volume of (plastic) waste, different synergistic effects occur during co-pyrolysis. Flash co-pyrolysis of willow and polylactic acid at 723 K results in an enhanced bio-oil yield with a lower water content and a higher calorific value. The synergistic effects are observed to increase along with the addition of PLA. Based on these conclusions, an appropriate biomass/PLA ratio can be proposed for each biomass. In this case study, the flash co-pyrolysis of 1:2 willow/PLA resulted in the most pronounced synergy: an increase of 28 % in bio-oil yield, a decrease of 37 % in water content, and an increase of 27 % in energy recuperation.

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