

ENERGY MINIMIZATION OF DISTILLATION COLUMNS BY ARTIFICIAL NEURAL NETWORKS

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1 WHAT?

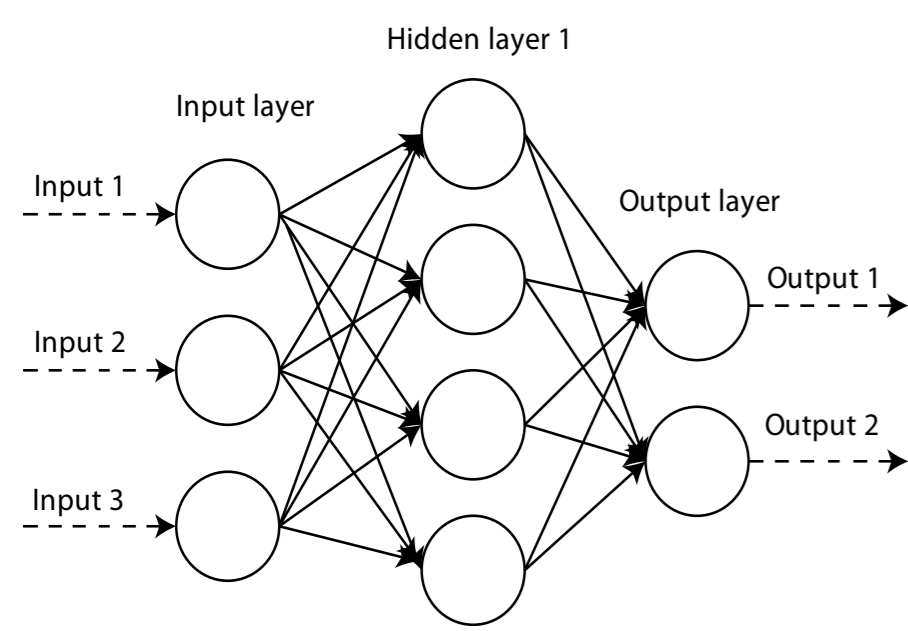


Figure 1: ANN structure

= Artificial Neural Network (ANN)

- Computing systems
- Allow for the detection of **non-linear relations** between features
- **Low simulation time** compared to chemical simulation software suites like Aspen Plus

2 PROBLEM DEFINITION

SUSTAINABILITY

- Design chemical installations with the goal of energy minimization
- **Energy minimization** → reduction of CO₂
- To design distillation columns in Aspen, a lot of simulations need to be performed
- ANN's reduce this simulation time and can provide a good **prediction** of the actual optimal settings.

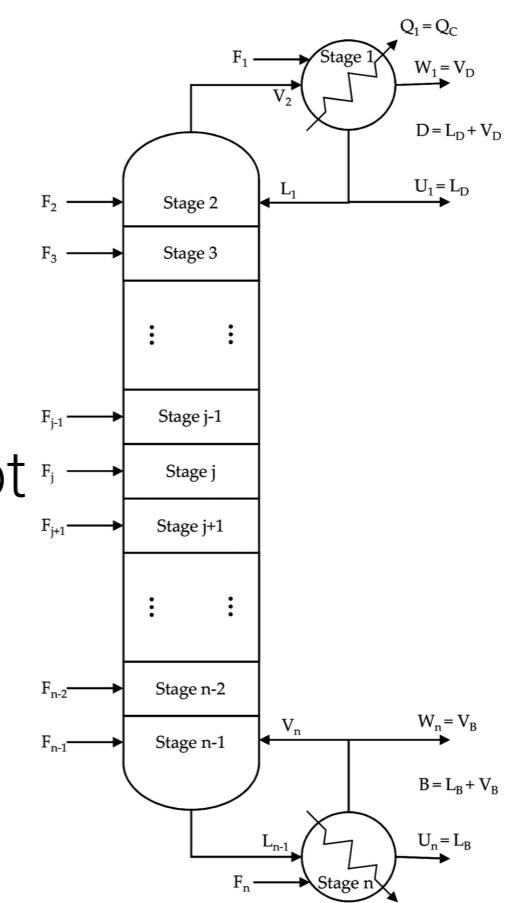


Figure 2: Distillation column [1,p.4]

4 TROUBLESHOOTING

IMBALANCED DATA PROBLEM

When performing simulations, data samples with a very pure distillate are overrepresented causing a bias during training.

Possible approaches:

- Redefining boundaries of input features
- Under-sampling
- Gathering more qualitative data

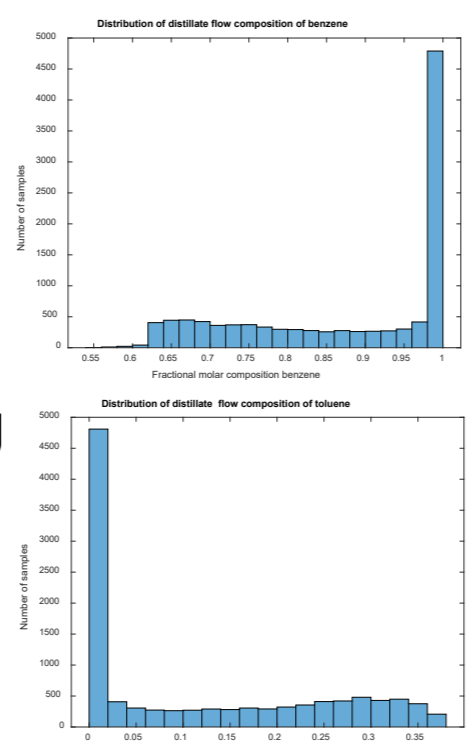


Figure 4: Distributions Of distillate flow rates

3 METHOD

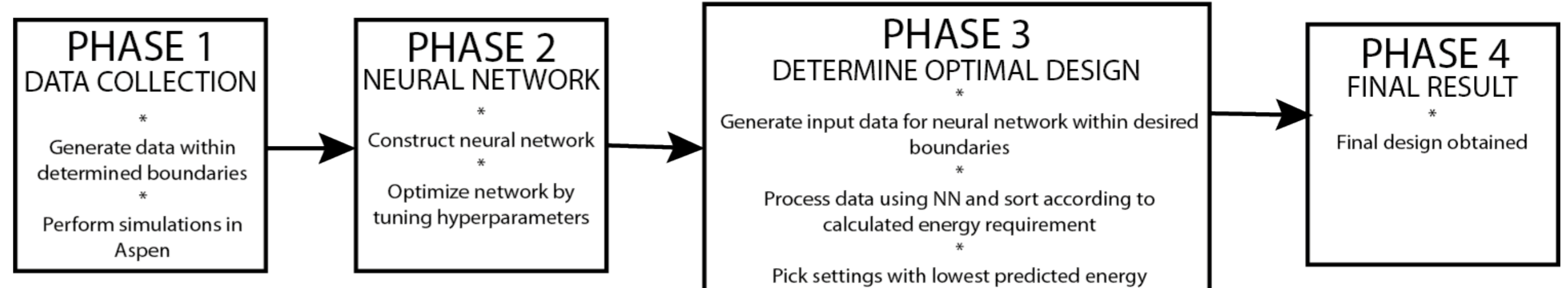


Figure 3: Methodology

5 RESULTS

CASE STUDY 1

Creating a model to find optimal design (reflux ratio, feed stage) and compare the result to the use of Driving Force Method given specific feed conditions [2]

	Neural network	Accuracy check ⁽¹⁾	DFM
No. of stages, Ns	21	21	21
No. of feed location, NF	15	13	13
Reflux ratio	1.3722	1.41	1.41
Composition at top			
Benzene	0.9900	0.9718	0.9900
Toluene	0.0100	0.0282	0.0100
p-xylene	0.0000	0.0000	0.0000
Composition at bottom			
Benzene	0.0415	0.0585	0.0415
Toluene	0.5714	0.5543	0.5714
p-xylene	0.3871	0.3871	0.3871
Energy condenser (kW)	933.6	937.3	953.9
Energy reboiler (kW)	1181.3	1182.9	1201.6
Total energy (kW)	2114.9	2120.2	2155.5

CASE STUDY 2

Expand model of first case study with number of stages, feed composition and feed temperature

	IMPURE FEED		PURE FEED	
	Neural network	Accuracy check	Neural network	Accuracy check
No. of stages, Ns	26	0.1832	17	0.0400
No. of feed location, NF	15	9	9	0.4007
Reflux ratio	0.4184	78.9628	0.4007	77.5054
Feed temperature (°C)				
Composition at top				
Benzene	0.9900	0.7964	0.9900	0.9593
Toluene	0.0100	0.1832	0.0100	0.0400
p-xylene	0.0000	0.0204	0.0000	0.0007
Composition at bottom				
Benzene	0.0286	0.1618	0.2540	0.3424
Toluene	0.5640	0.4503	0.5523	0.4661
p-xylene	0.4074	0.3880	0.1937	0.1916
Energy condenser (kW)	423.2	452.8	836.4	851.8
Energy reboiler (kW)	682.1	694.0	983.3	996.3
Total energy (kW)	1105.3	1146.8	1819.7	1848.1

6 CONCLUSION & FUTURE WORK

- Model performs well in predicting the required energy for the separation
- Imbalanced data set needs to be taken into account when gathering data
- The model needs to have the reflux ratio at the output, together with the reboiler and condenser duty.
- Further optimization of the model needs to be performed by varying other hyperparameters

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[1] V. Steffen and E. A. da Silva, "Steady-State Modeling of Equilibrium Distillation," in *Distillation - Innovative Applications and Modeling*, InTech, 2017.

[2] M. Faris, A. Noor, F. Mohd, I. Asri, I. Norazana, and K. Mohd, "Design of Energy Efficient Distillation Columns Systems," in *International symposium on green manufacturing and applications*, 2014, no. June, pp. 66–69.

(1) The accuracy check is performed to see if the calculated values of the ANN correspond to the values that are found in Aspen.